

A0371



ConocoPhillips Company
1230 W. Washington Street, Suite 212
Tempe, AZ 85281

November 6, 2006

Mr. Donald Hwang
Alameda County Environmental Health Services
1131 Harbor Bay Parkway, Suite 250
Alameda, CA 94502

Alameda County
NOV 09 2006
Environmental Health

RE: Document Transmittal
Fuel Leak Case
76 Station # 7004
15599 Hesperian Blvd., San Leandro, CA

Dear Mr. Hwang:

Please find attached SECOR's *Addendum to Quarterly Status and Remediation Summary Report - Second Quarter 2006* dated November 6, 2006 for the above referenced site. I declare under penalty of perjury that to the best of my knowledge the information and/or recommendations contained in the attached proposal or report are true and correct.

If you have any questions or need additional information, please call me at (602) 452-2507.

Sincerely,

James F. Trotter
Site Manager
Risk Management & Remediation
ConocoPhillips Company

Enclosure

cc: Diane Barclay, SECOR



SECOR
INTERNATIONAL
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November 6, 2006

Mr. Donald Hwang
Alameda County Environmental Health Services
1131 Harbor Bay Parkway Suite 250
Alameda, CA 94502

RE: Addendum to Quarterly Status and Remediation Summary Report – Second Quarter 2006

Former 76 Service Station No. 7004
15599 Hesperian Boulevard
San Leandro, California
SECOR Project No.: 77CP.01631.00.0304

Dear Mr. Hwang:

SECOR International Incorporated (SECOR) is submitting this Addendum to supplement the *Quarterly Summary Report, Second Quarter 2006*, dated August 30, 2006, for the subject site. This Addendum is presented to clarify the groundwater gradient discussion, and to present revised engineering calculations.

In the discussion section of the quarterly report, SECOR indicated that the radially inward groundwater gradient evaluated by TRC (*Quarterly Monitoring Report, April through June 2006, dated June 20, 2006*) for the second quarter was likely due to operation of the temporary dual-phase extraction (DPE) system at the site, and that the system was operational during the May 25, 2006 monitoring and sampling event. While the DPE system had been previously operating at the site, and had been using wells MW-5, MW-3, and RW-1 as extraction wells, it had been shut down and was not fully operational again until the week following the May 25 monitoring and sampling event. Inspection of field data sheets in the TRC report indicated that the radially inward gradient reported by TRC was evaluated using depths to water from MW-3 and MW-5 that had been measured after other site wells were purged and sampled. It is possible that the water elevations from wells MW-3 and MW-5 were affected by this purging and sampling, and SECOR believes that this gradient evaluation may not be representative of actual site conditions prior to purging on May 25, 2006. Evaluation of the gradient without using these two data points indicated flow that varied from northwest to southeast.

SECOR revised engineering Tables 2, 3, 4, and 7 and Figures 3 and 5 of the Quarterly Report. The revised tables and figures are included in Attachment A. During the second quarter, the DPE system was approximately 21 percent operational, and ran for approximately 380 hours. Through groundwater extraction (GWE), the system removed an approximate total of 0.107 pounds (0.017 gallons) of TPHg, 0.019 pounds (0.003 gallons) of MTBE, and 0.009 pounds (0.001 gallons) of TBA. Soil vapor extraction (SVE) removed approximately 1.86 pounds (0.31 gallons) of TPHg, and 0.07 pounds (0.01 gallons) of MTBE. Through GWE, a total of approximately 115,340 gallons of water have been removed since system startup. The DPE

SECOR

Mr. Donald Hwang
November 6, 2006
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system (GWE and SVE combined) removed approximately 1.967 pounds (0.327 gallons) of TPHg, 0.089 pounds (0.013 gallons) of MTBE, and 0.009 pounds (0.001 gallons) of TBA.

If you have any questions or comments regarding the contents of this document, please contact the undersigned at (916) 861-0400.

Sincerely,
SECOR International Incorporated



Diane Barclay, C.H.G.
Senior Geologist



Adrian Pérez, P.E.
Associate Engineer



Attachment Revised Tables and Figures

cc: Mr. Thomas Kosel, ConocoPhillips
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Mr. Bob Clark-Riddell, Pangea Environmental Services, Inc, 1710 Franklin Street, Suite 200, Oakland, CA 94612

ATTACHMENT
REVISED TABLES AND FIGURES

Addendum to Quarterly Status and Remediation Summary Report – Second
Quarter 2006

Former 76 Service Station No. 7004
15599 Hesperian Boulevard
San Leandro, California

SECOR Project No.: 77CP.01631.00.0304
November 6, 2006

**Table 2
Temporary Dual Phase Extraction System-Operating Data**

Former 78 Station #7004
15599 Hesperian Blvd
San Leandro, California

Date	Notes	Hourmeter Reading (hours)	Totalizer Reading (gallons)	Well Field Temperature (°F)	System Vacuum (inHg)	Flow Rate (acfm)	Flow Rate (scfm) [1]	MW-3 FID (ppmv)	MW-5 FID (ppmv)	RW-1 FID (ppmv)	Well Field FID (ppmv)
3/20/08	a	12,078.5	43,900	80	28	57.0	8	51.1	60.2	15.0	60
3/27/08		12,099.8	54,000	80	28	62.9	9	398	187	17.9	389
4/10/08	b,c	12,345.4	90,210	80	25	78.5	13	51	385	87.2	59.1
4/17/08	d	12,464.8	114,700	--	--	--	--	--	--	--	--
6/1/08	e	12,464.8	114,700	79.1	25	77.2	13	380.2	140.0	14.0	375
6/5/08	f	12,557.7	126,390	78.1	25	70.1	11	109	75 F/O	25 F/O	100 F/O
6/9/08		12,581.9	131,450	--	--	--	--	--	--	--	--
6/12/08		12,604.2	136,030	--	--	--	--	--	--	--	--
6/22/08	g	12,850.0	145,670	75.2	25	68.2	11	104.2	4.2	7.5	103
6/28/08	h	12,725.8	159,240	98	25	71.2	11	--	--	--	--

REPORTING PERIOD: Second Quarter

Period Operation (hours):	380
Period Operational (%):	21%
Period Extracted (gals):	89,030
Period Average Discharge Rate (gpm):	3.0
Total Operation (hours):	649
Total Operation (%):	28%
Total Liquid Extracted Historical (gals):	115,340
Average Historical Discharge Rate (gpm):	3.0

Definitions:

--	Data not available or not applicable
ATC	Authority to Construct
acfm	Actual cubic feet per minute
°F	Degrees Fahrenheit
FID	Flame Ionization Detector
F/O	Flame Out
ft ³	Cubic feet
InHg	Inches of mercury
ppmv	Parts per million by volume
scfm	Standard cubic feet per minute
gals	Gallons
[]	Indicates reference to equation
gpm	Gallons Per Minute

Equations:

[1]
$$SCFM = \frac{ACFM \cdot T_{std} \cdot (P_{abs})}{(460 + T) \cdot P_{atm}}$$

T_{std} Temperature at standard conditions (528 Rankine)
P_{abs} Atmospheric pressure at standard conditions minus manifold vacuum (inHg)
P_{atm} Atmospheric pressure at standard conditions (29.92 inHg)
T Manifold vapor temperature reading (°F).

Notes:

- a = system start-up on 3/20/08
- b = effluent reporting limits are assumed as the effluent concentration; vapor control system efficiency equation is not an accurate reflection of actual system efficiency
- c = system down and restarted, set slurp tubes to top of casing
- d = system down, generator unoperational and needs to be replaced
- e = new generator installed and system restarted
- f = system down, high level switch on baker tank triggered shut down of system on 6/4/08, system restarted
- g = system resampled on 6/21/08 w/ less 10 ppmv reporting limits
- h = system down, generator shut down due to high water temperature, system cooled down and restarted

Permits:

Air emissions are permitted under Bay Area Air Quality Management District Application Number 13031 and MTS Plant Number 13708.

Table 3
Temporary Dual Phase Extraction System - Soil Vapor Influent Analytical Data and Mass Recovery

Former 76 Station #7004
 15599 Heeperton Blvd
 San Leandro, California

Date Sampled	Sample ID	Notes	Hour Meter Reading (hours)	Well Field Flow Rate (achm)	Influent Concentrations							TPHg Recovery			Benzene Recovery			MBE Recovery			
					TPHg (ppmv)	Benzene (ppmv)	Toluene (ppmv)	Ethyl-benzene (ppmv)	Total Xylenes (ppmv)	MBE (ppmv)	VOC (ppmv)	Recovery Rate (lb/day) [1]	Period Net Recovery (lbs) [2]	Cumulative Recovery (lbs) [3]	Recovery Rate (lb/day) [1]	Period Net Recovery (lbs) [2]	Cumulative Recovery (lbs) [3]	Recovery Rate (lb/day) [1]	Period Net Recovery (lbs) [2]	Cumulative Recovery (lbs) [3]	
3/20/2006	INF		12077	12	15	<0.31	<0.26	<0.23	<0.23	0.48	<16.4	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	
4/10/2006	INF		12,345.4	13	<14	<0.31	<0.26	0.27	<0.23	0.67	<15.7	0.07	0.79	0.79	0.00	0.00	0.00	0.00	0.03	0.03	
6/5/2006	INF		12,557.7	11	24	<0.31	<0.26	<0.23	<0.23	0.93	<25.2	0.10	0.92	1.71	0.00	0.00	0.00	0.00	0.03	0.06	
6/22/2006	INF		12,725.8	11	5.1	<0.02	0.031	<0.02	<0.02	0.67	<5.86	0.02	0.15	1.86	0.00	0.00	0.000	0.00	0.02	0.07	
REPORTING PERIOD: Second Quarter																					
Period Pounds Removed [4]:													1.86			0.00		0.07			
Period Gallons Removed [5]:													0.31			0.00		0.01			
Total Pounds Removed [6]:													1.86			0.00		0.07			
Total Gallons Removed [7]:													0.31			0.00		0.01			

Definitions:

- lb Pounds
- MBE Methyl tert-butyl ether
- ppmv Parts per million by volume
- scfm Standard cubic feet per minute
- TPHg Total petroleum hydrocarbons as gasoline
- VOC Volatile organic compound

Notes:

Molecular Weights:

- TPHg 102 g/mol
- Benzene 78 g/mol
- MBE 88 g/mol

Densities:

- TPHg 0.22 lbs/ft³
- Benzene 0.2027 lbs/ft³
- MBE 0.2268 lbs/ft³

Vapor densities are at 1 atmosphere and 68 degrees Fahrenheit

Equations:

$$[1] \text{ Recovery Rate } \left(\frac{\text{lb}}{\text{day}} \right) = \frac{\text{Concentration (ppmv)} \cdot \text{Molecular Weight} \cdot \text{Flow} \left(\frac{\text{ft}^3}{\text{min}} \right) \cdot 60 \left(\frac{\text{min}}{\text{hour}} \right) \cdot 24 \left(\frac{\text{hour}}{\text{day}} \right)}{V_{\text{mol}} (\text{ft}^3) 10^4}$$

$$[2] \text{ Period Net Recovery (lbs)} = \frac{\text{Recovery Rate} \left(\frac{\text{lb}}{\text{day}} \right) \cdot (\text{Hour Meter Reading}_i - \text{Hour Meter Reading}_{i-1}) (\text{hour})}{24 \left(\frac{\text{hour}}{\text{day}} \right)}$$

$$[3] \text{ Cumulative Recovery (lbs)} = \sum \text{Period Net Recovery (lbs)}$$

$$[4] \text{ Period Pounds Removed (lbs)} = \text{Reporting Period Net Recovery (lbs)}$$

$$[5] \text{ Period Gallons Removed (gallons)} = \frac{\text{Period Pounds Removed (lbs)}}{\text{Density} \left(\frac{\text{lb}}{\text{gal}} \right)}$$

$$[6] \text{ Total Pounds Removed (lbs)} = \text{Cumulative Recovery (lbs)}$$

$$[7] \text{ Total Gallons Removed (gallons)} = \frac{\text{Total Pounds Removed (lbs)}}{\text{Density} \left(\frac{\text{lb}}{\text{gal}} \right)}$$

V_{mol} = Volume of 1.0 mole of an ideal gas is 386.6 ft³ at 70°F and 29.92 inHg

Table 4
Temporary Dual Phase Extraction System - Soil Vapor Emissions Data

Former 76 Station #7004
 15599 Hesperian Blvd
 San Leandro, California

Date Sampled	Sample ID	Notes	Hour Meter Reading (hours)	Total System Flow Rate (scfm)								VOC Emissions		Benzene Emissions	
					TPHg (ppmv)	Benzene (ppmv)	Toluene (ppmv)	Ethyl-benzene (ppmv)	Total Xylenes (ppmv)	MTBE (ppmv)	VOC (ppmv)	Emissions Rate (lbs/day)	Cumulative Emissions (lbs)	Emissions Rate (lbs/day)	Cumulative Emissions (lbs)
3/20/2006	EFF	a,b	12,076.5	12	<14	<0.31	<0.26	<0.23	<0.23	<0.14	<15.17	0	0	0	0
4/10/2006	EFF		12,345.4	13	<14	<0.31	<0.26	<0.23	<0.23	<0.14	<15.17	0.07	0.82	0.001	0.01
6/5/2006	EFF		12,557.7	11	<14	<0.31	<0.26	<0.23	<0.23	<0.14	<15.17	0.07	1.46	0.001	0.02
6/22/2006	EFF	c	12,725.8	11	1.8	<0.020	0.022	<0.020	<0.020	<0.020	<1.90	0.01	1.59	0.000	0.02

Definitions:

-- Data not available
 lbs Pounds
 MTBE Methyl tert-butyl ether
 ppmv Parts per million by volume
 scfm Standard cubic feet per minute
 TPHg Total petroleum hydrocarbons as gasoline
 VOCs Volatile organic compounds as measured with a Flame Ionization Detector

Permit Conditions (Application No. 13031):

VOC Control Efficiency > 98.5% (For inlet concentrations \geq 2000 ppmv)
 VOC Control Efficiency > 97% (For inlet concentrations \geq 200 ppmv and < 2000 ppmv)
 VOC Control Efficiency > 90% (For inlet concentrations < 200 ppmv)
 VOC Control Efficiency Waived for Outlet Efficiencies < 10 ppmv

Notes:

- a = system start-up
- b = effluent reporting limits are assumed as effluent concentration; vapor control system efficiency is not an accurate reflection of system efficiency
- c = outlet efficiencies less than 10 ppmv
- * we have assumed the detection limits to provide a maximum estimate for vapor emissions to the atmosphere, which is a conservative estimate

Table 7
Temporary Dual Phase Extraction System - Groundwater Mass Recovery

CP 7004
15500 Hesperian Blvd
San Leandro, California

Influent			Influent Concentrations				TPHq Recovery			Benzene Recovery			MIBE Recovery			TBA Recovery						
Date Sampled	Sample ID	Notes	Hour Meter Reading (hours)	Totalizer Reading (gallons)	PHR60 Volume Extracted (gallons)	TPHq (µg/L)	Benzene (µg/L)	MIBE (µg/L)	TBA (µg/L)	Absorption Rate (lbs/day) [1]	Period Net Adsorbed (lbs) [2]	Cumulative Adsorbed (lbs) [3]	Absorption Rate (lbs/day) [1]	Period Net Adsorbed (lbs) [2]	Cumulative Adsorbed (lbs) [3]	Absorption Rate (lbs/day) [1]	Period Net Adsorbed (lbs) [2]	Cumulative Adsorbed (lbs) [3]	Absorption Rate (lbs/day) [1]	Period Net Adsorbed (lbs) [2]	Cumulative Adsorbed (lbs) [3]	
3/20/2006	KD		12076.5	43,900	—	280	<0.5	38	18	0.000	0.000	0.000	0.000	0.000	0.000	0.0000	0.000	0.000	0.0000	0.000	0.000	0.000
4/10/2006	KD		12345.4	90,210	46,310	58	<0.50	13	14	0.005	0.061	0.061	0.000	0.000	0.000	0.0007	0.009	0.009	0.0008	0.000	0.000	0.000
6/5/2006	KD		12557.7	128,290	36,180	180	<0.50	38	10	0.005	0.045	0.107	0.000	0.000	0.000	0.0012	0.011	0.019	0.0003	0.000	0.000	0.000
REPORTING PERIOD: Second Quarter																						
Period Pounds Removed [4]:										0.107			0.000			0.018			0.009			
Period Gallons Removed [5]:										0.017			0.000			0.003			0.001			
Total Pounds Removed [6]:										0.107			0.000			0.018			0.009			
Total Gallons Removed [7]:										0.017			0.000			0.003			0.001			

Definitions:

- lbs Pounds
- MIBE Methyl tert-butyl ether
- NA Not sampled or not analyzed
- TBA Tert-butyl alcohol
- TPHq Total petroleum hydrocarbons as gasoline
- (µg/L) micrograms per Liter
- KD Knockout

Notes:

Physical Properties:

- Density of gasoline = 6.1 pounds per gallon
- Density of diesel = 7.18 pounds per gallon
- Density of motor oil = 7.82 pounds per gallon
- Density of benzene = 7.4 pounds per gallon
- Density of MIBE = 6.18 pounds per gallon
- Density of TBA = 6.8 pounds per gallon

Equations:

- [1] Removal Rate $\left(\frac{\text{lbs}}{\text{day}}\right) = \frac{\text{Period Net Removed (lbs)} \cdot 24 \left(\frac{\text{hour}}{\text{day}}\right)}{(\text{Hour Meter Reading}_2 - \text{Hour Meter Reading}_1)}$
- [2] Period Net Removed (lbs) = (Concentration) $\left(\frac{\text{µg}}{\text{L}}\right) \cdot 3.785 \left(\frac{\text{L}}{\text{gallon}}\right) \cdot 2.205 \times 10^{-9} \left(\frac{\text{lbs}}{\text{µg}}\right) \cdot \text{Period Extracted (gallons)}$
- [3] Cumulative Removed (lbs) = (Period Net Removed) (lbs) + Cumulative Removed (lbs)
- [4] Period Pounds Removed (lbs) = \sum Period Net Removed (lbs)
- [5] Period Gallons Removed (gallons) = $\frac{\text{Period Pounds Removed (lbs)}}{\text{Density of Constituent 1} \left(\frac{\text{lbs}}{\text{gallon}}\right)}$
- [6] Total Pounds Removed (lbs) = Cumulative Adsorbed (lbs)
- [7] Total Gallons Removed (gallons) = $\frac{\text{Total Pounds Removed (lbs)}}{\text{Density of Constituent 1} \left(\frac{\text{lbs}}{\text{gallon}}\right)}$

In order to show best estimate, recovery calculations assume one-half of the laboratory reporting limit when an analyte is reported as non-detect.

Figure 3
Temporary DPE Soil Vapor Mass Recovery

CP 7004
15599 Hesperian Blvd
San Leandro California

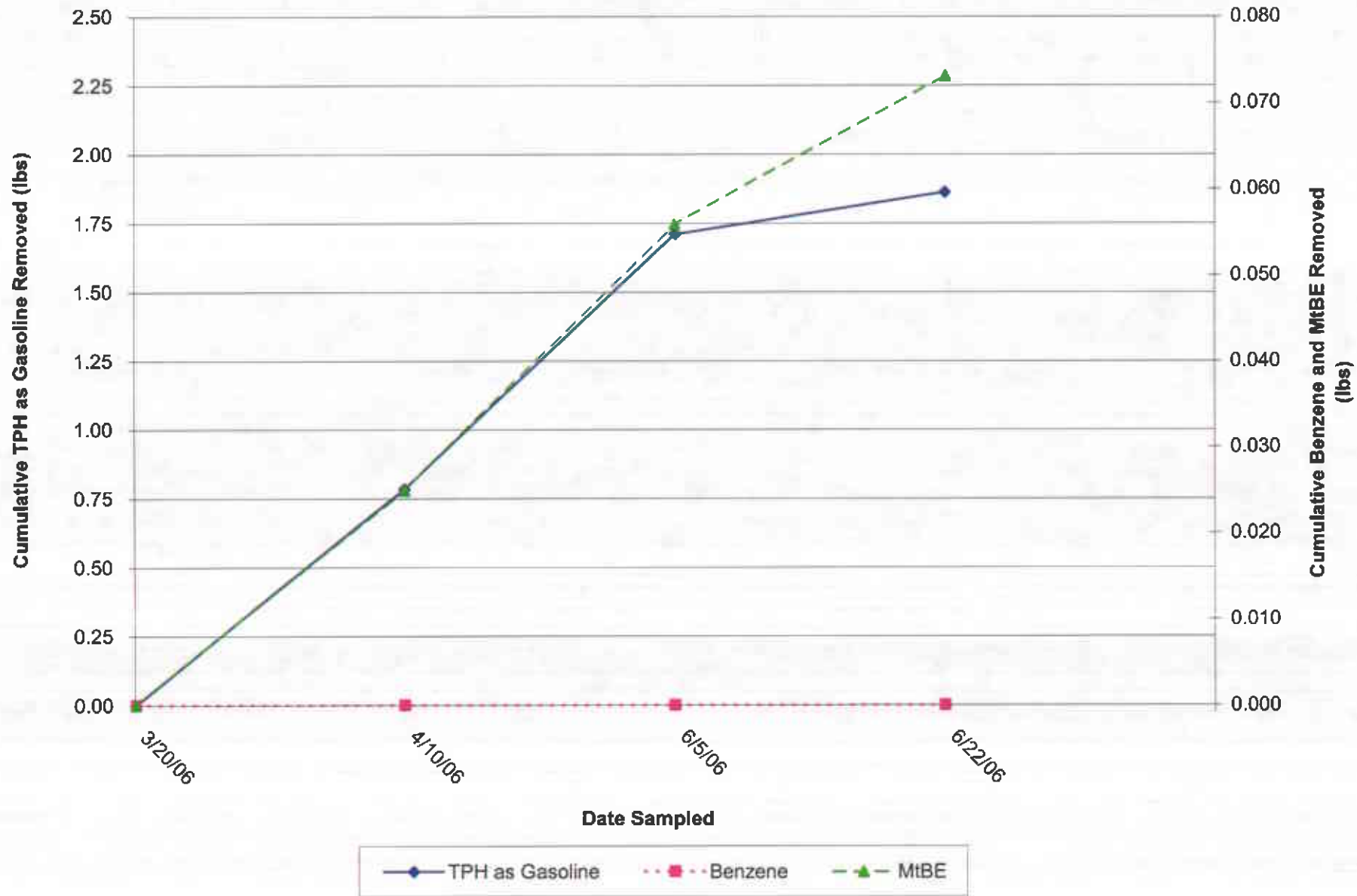


Figure 5
Temporary DPE Groundwater Mass Recovery

CP 7004
15599 Hesperian Blvd
San Leandro, California

