



November 18, 1995

Chevron U.S.A. Products Company 6001 Bollinger Canyon Rd , Bldg L P.O Box 5004 San Ramon, CA 94583-0804

Mark A. Miller SAR Engineer Phone No. 510 842-8134 Fax No. 510 842-8252

Ms. Jennifer Eberle Alameda County Health Care Services Department of Environmental Health 1131 Harbor Bay Parkway, Suite 250 Alameda, CA 94502-6577

Re: Former Chevron Service Station #9-4816 301 14th Street, Oakland, CA

Dear Ms. Eberle:

Enclosed is the System Startup Report dated October 20, 1995, prepared by our consultant Terra Vac Corporation for the above referenced site. The report documents the progress of the remedial system. Similar update report will be forwarded to your office on a monthly basis until remediation is completed.

If you have any questions or comments, please feel free to contact me at (510) 842-8134.

Sincerely,

CHEVRON U.S.A. PRODUCTS COMPANY

Mark A. Miller

Site Assessment and Remediation Engineer

Enclosure

cc: Mr. Tim Warner, Terra Vac

Mr. J.N. Robbins, CHVPK/V1156

Ms. B.C. Owen

Ms. Beth D. Castleberry Gray, Cary, Ware & Freidenrich 400 Hamilton Avenue Palo Alto, CA 94301-1825



■ TEL (510) 351-8900

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October 20, 1995

Mr. Mark Miller Chevron U.S.A. Products Company 6001 Bollinger Canyon Road San Ramon, California 94583

Re: System Startup Report

Former Chevron Station 9-4816

301 14th Street Oakland, California

Dear Mr. Miller:

Enclosed please find the startup report for remediation operations at the above referenced site. This report includes operating data, duration, rates of hydrocarbon removal, cumulative pounds removed to date and air permit compliance information.

If you have any questions, please feel free to call.

Sincerely, Terra Vac Corporation

Jason L. Nutt Staff Engineer

Enclosure

cc: File 30-0220.20

Timothy M. Warner Project Manager

SYSTEM STARTUP REPORT FORMER CHEVRON STATION 9-4816 301 14TH STREET OAKLAND, CALIFORNIA

1.0 Background

Terra Vac has been contracted by Chevron U.S.A. Products Company (Chevron) to install and operate a soil and groundwater remediation system at the above referenced site (Figure 1). The purpose of this report is to provide data on system startup, operation, and source test data for the first week of operation.

2.0 Startup

The Global 750 catalytic oxidizer was activated on Tuesday, October 3, 1995. Before operations began, all equipment and control systems were checked for proper operation. The equipment being utilized at the site is as follows:

Vapor Abatement System: To meet the requirements of the air pollution control district, and Global 750 catalytic oxidizer was mobilized to the site. This unit is operating on 208 volt, 3 phase service, and uses propane as supplemental fuel.

A 30 horsepower Lamson Turbotron will supply the necessary soil vacuum. The extraction equipment is integrated as part of the Global 750 and is equipped with an explosion proof motor, motor controls, and noise suppression devices.

A 150-gallon vapor-liquid separator has been integrated into the system and is mounted on the Global 750 trailer. This separator has both high and high-high water level controls that operate the water pump and shut the system down, respectively.

Air Injection System: A 15 horsepower oil-free blower was mobilized to the site to enhance naturally occurring biodegradation. Since no free product was encountered during startup, this system is operating in conjunction with the vapor abatement system.

3.0 Operations

Initial testing and safety check out of the system took place on October 2, 1995, and actual startup occurred on October 3, 1995. A source test was conducted to verify air permit compliance and destruction efficiency. Upon successful completion of the source test, Terra Vac

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was given verbal approval to operate prior to receipt of the permit to operate document. Operating data is shown in Table 1, and efficiency data is presented as Table 2.

Due to high water yield, seven of the ten extraction wells were brought on-line the first day. Initial extraction rates were approximately 34 pounds of petroleum hydrocarbons per day (lbs/day), which rapidly increased to an extraction rate of 660 lbs/day. Based on analyses of inlet vapor samples through October 17, 1995, approximately 3,854 pounds, or 640 gallons, of hydrocarbon have been removed from the subsurface. A graph showing removal rate versus time is attached as Figure 2, and a graph showing cumulative pounds of hydrocarbons removed is attached as Figure 3.

Table 3 shows the individual wellhead concentrations and Table 4 shows the vapor stream components of representative on-line wells utilizing BTEX compounds for fractional cuts. Percentages above 60 percent in the benzene and lighter range usually indicate proximity to relatively fresh product or that the well is drawing from a distant source. To monitor the progress of remediation, Terra Vac will track the decline in the percentage of vapors lighter than benzene.

The remediation system has operated for 14.1 days, with only minor shut downs caused by high liquid level in the knock-out pot (KO) and high LEL. In all cases, the problem was quickly remedied and the system restarted.

4.0 Air Permit Compliance

As per Bay Area Air Quality Management District (BAAQMD) requirements, an on-site source test was conducted between October 3, and October 10. Samples were taken from the inlet and outlet of the abatement device to determine destruction efficiencies at the documented flow rate and stack temperature. Bag samples were taken for five consecutive working days and analyzed in the Terra Vac office laboratory for TPH-g and BTEX via modified EPA methods 8015/8020.

After the first week of operation, samples will be taken and analyzed on a weekly basis for a one month period, after which Terra Vac will sample bi-monthly for the length of the project.

Destruction efficiencies for the first week are presented in Table 2, and demonstrates that the unit is maintaining a destruction efficiency of greater than 99 percent when inlet concentrations are below 2000 parts per million by volume. The resulting destruction efficiencies meet the requirements set by the BAAQMD.

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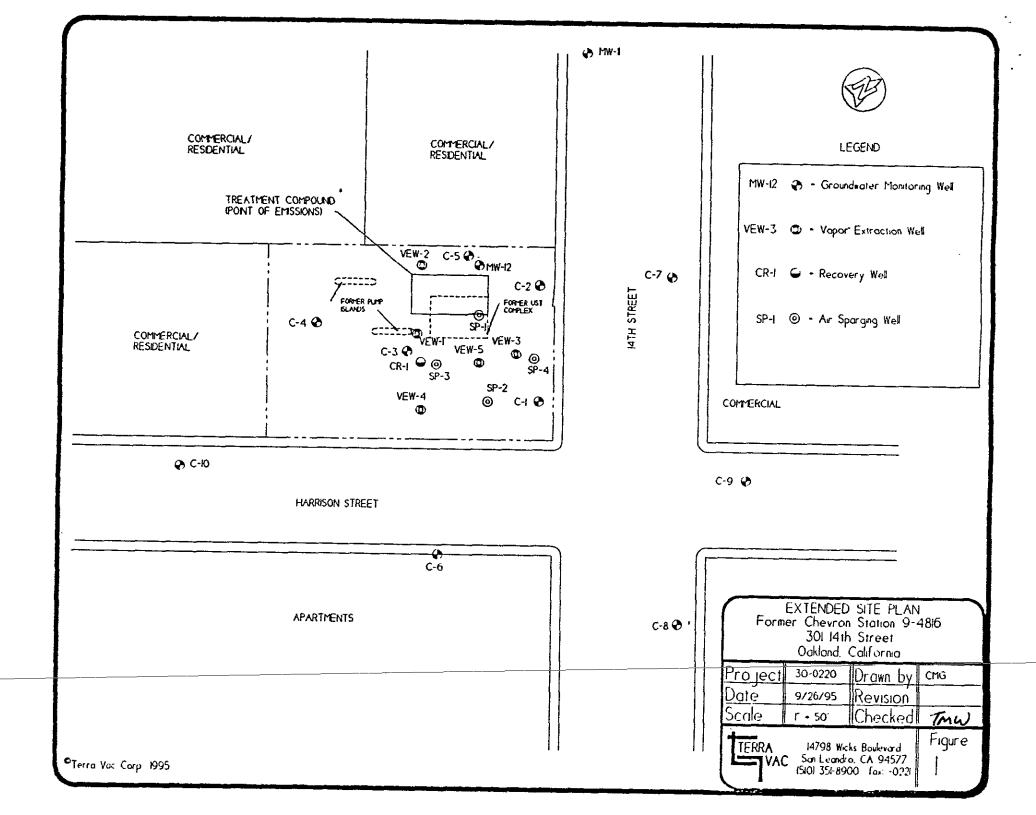


Figure 2 Removal Rate

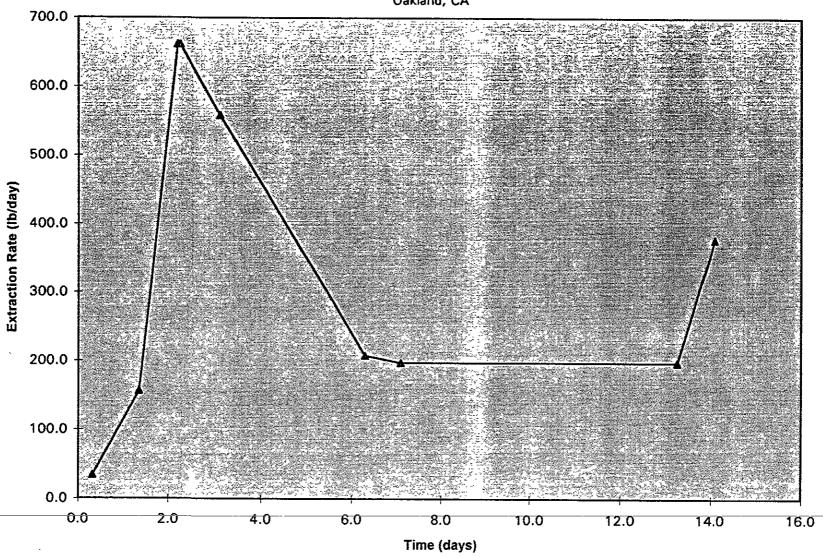


FIGURE 3
Cumulative Removal Rate

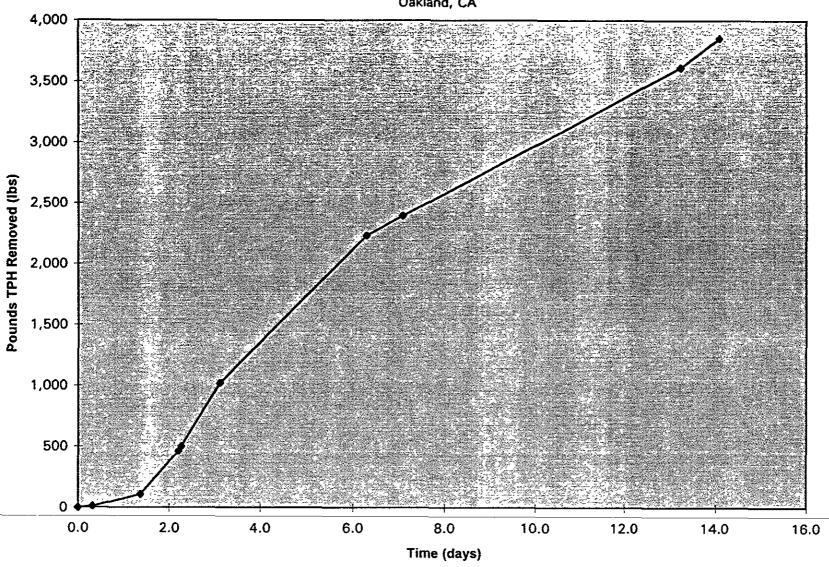


Table 1 Operation Summary

	Kalangangan Seria. Paggangan Seria	er skrådet i Sammer det det	Extracted			Cumulative	Cumulative	
	Run Time	andere in Marie Andere in Marie	Flow	Conc.	Rate	Extraction	: Water	
Date	ः (days)	Sample	(scfm)	(mg/l)	(lb/day)	(lb)	(gal)	
10/03/95	0.0	start	558			0		
10/03/95	0.3	1	558	0.68	34.1	11	0	
10/04/95	1.4	3	507	3.44	156.6	109	0	
10/05/95	2.2	5	596	12.36	661.5	462	4,270	
10/05/95	2.3	stop	0		661.5	501	4,270	
10/06/95	2.3	start	538		661.5	501	4,270	
10/06/95	3.1	7	467	13.31	558.1	1,019	4,412	
10/09/95	6.3	9	307	7.56	208.3	2,234	16,360	
10/10/95	7.1	11	385	5.72	197.6	2,396	22,264	
10/16/95	13.3	nst	447		197.6	3,612	58,340	
10/17/95	14.1	23	447	9.41	377.6	3,854	65,070	
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Table 2 Operation Summary

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Former Chevron Station 9-4816 301 14th Street Oakland, CA

Date		Outlet :			Benzene	Emissi	Abatement	
	Run Time (days)	Temp Flow (deg F) (scfm		Conc (mg/l)	Conc (mg/l)	pounds per day POC Benzene		Efficiency
·· Date · · ·	:::\toays/	tueg (7.	(SCIIII)	e cogni, o	ារ អម្សាក្សៈនេះ	· · · · · · · · ·	. Benzene .	(%)
10/03/95	0.3	598	658	0.016	0.002	0.95	0.12	97.23
10/04/95	1.4	720	607	0.100	0.002	5.45	0.11	96.52
10/05/95	2.2	1135	696	0.003	0.002	0.19	0.13	99.97
10/06/95	3.1	1186	567	0.045	0.002	2.29	0.10	99.59
10/09/95	6.3	855	397	0.012	0.002	0.43	0.07	99.79
10/10/95	7.1	868	449	0.018	0.002	0.73	0.08	99.63
10/17/95	14.1	600	511	0.188	0.002	8.63	0.09	97.72

Notes:

1.) Detection limit = 0.002 mg/l

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Table 3 Operation Summary

Tere ∰ 4 : Date (10/17/95
CR-1	
lighter than benzene	61%
benzene to toluene	24%
toluene to xylene	12%
heavier than xylene	3%
C-1	
lighter than benzene	34%
benzene to toluene	36%
toluene to xylene	24%
heavier than xylene	6%
C-2	
lighter than benzene	62%
benzene to toluene	19%
toluene to xylene	9%
heavier than xylene	10%
C-5	
lighter than benzene	61%
benzene to toluene	24%
toluene to xylene	11%
heavier than xylene	4%
	. , , ,
VEW-4	
lighter than benzene	36%
benzene to toluene	35%
toluene to xylene	19%
heavier than xylene	10%
INLET	
lighter than benzene	39%
benzene to toluene	25%
toluene to xylene	25%
heavier than xylene	11%

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Table 4 Operation Summary

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Well	CR-1	C ₅ 1:::	C-2	C-3	C-5	VEW-1	VEW-2	VEW-3	VEW-4	VEW-5	inlet		
10/17/95	9.93	25.17	6.24	9.93	10.01	6.19	4.47	11.89	5.36	11.95	9.41		