ACCURATE TANK TESTING inc.

P.O. BOX 163 • ANTIOCH, CA 94509

(415) 754-9853 (415) 754-9935

CAL LICENSE NO. 481444

Yes FUEL TANKS

To: _____

PROPOSAL

Gentlemen: _____

Date: [illegible] 1986

Project: Test underground Fuel Tanks

We propose to do the following work:

1. [illegible] 1 - 10,000 gal. diesel fuel tank. ($350.00)

2. [illegible] 1,000 gal. gasoline tanks. ($350.00 ea.)

3. Tanks must be completely full, prior to our arrival upon the scheduled test date.

RECEIVED
OCT 23 1986
ENVIRONMENTAL HEALTH
ADMINISTRATION

For the sum of ($ 1,050.00) all in accordance with plans and specs., excepted as noted, and subject to the terms and provisions on the reverse side.

ACCEPTED: _____

ACCURATE TANK TESTING

By: _____

ACCURATE TANK TESTING
P.O. Box 163
Antioch, CA 94509
(415) 754-9853 (415) 754-9935

Cal. License No. 481444

SERVICE INVOICE

BILL TO [illegible] JOB LOCATION [illegible]

TERMS: A FINANCE CHARGE OF 1½% PER MONTH (ANNUAL RATE OF 18%) WILL BE CHARGED ON BALANCES OVER 30 DAYS.

DATE	SOLD BY	☒ CASH	☐ C O D	☐ CHARGES	☐ MDSE. RETD.
[illegible]	[illegible]				

QUANTITY	DESCRIPTION	PRICE	AMOUNT
2	Testing 2-1,000 gal. fuel tanks.		700.00
	2 man hours at $42.00 per hr. For work performed on diesel dispenser.		84.00

DESCRIPTION OF WORK		MON.	TUES.	WED.	THURS.	FRI.	SAT.	SUN.	TOTAL
	P								
	H								

SIGNED

MATERIAL	
SALES TAX	
TOTAL	784.00
L S POWER UNIT	
LABOR	
TOTAL AMOUNT	784.00

PLEASE PAY FROM THIS INVOICE. NO OTHER STATEMENT WILL BE RENDERED

TOTAL DUE UPON RECEIPT

Data Chart for Tank System Tightness Test

petro Tite
TANK TESTER

PLEASE PRINT

1. OWNER Property ☒ Tank(s) ☐

SUNOL CHEVRON | 11727 MAIN ST. | SUNOL | 862-2353
Name | Address | Representative | Telephone

Name | Address | Representative | Telephone

2. OPERATOR

ROCKY CAROTHERS
Name | Address | Telephone

3. REASON FOR TEST (Explain Fully)

COMPLIANCE WITH UNDERGROUND TANK REGULATIONS

4. WHO REQUESTED TEST AND WHEN

ROCKY CAROTHERS | Title | Company or Affiliation | 8-1-86
Name | Date

Address | Telephone

5. WHO IS PAYING FOR THIS TEST?

SUNOL CHEVRON | Person Authorizing | Title | Telephone
Company, Agency or Individual

Billing Address | City | State | Zip

Attention of | Order No | Other Instructions

6. TANK(S) INVOLVED

Identify by Direction	Capacity	Brand/Supplier	Grade	Approx Age	Steel/Fiberglass
#1	1000	CHEVRON	UNLEAD	10 yrs	STL
#2	1000	CHEVRON	REG.	10 yrs	STL
#3	550	CHEVRON	DIESEL	10 yrs	STL

7. INSTALLATION DATA

Location	Cover	Fills	Vents	Siphones	Pumps
EAST SIDE OF STATION	ASPHALT	1½	2"	N/A	SUCT.
North inside driveway, Rear of station, etc.	Concrete, Black Top, Earth, etc.	Size, Titefill make Drop tubes, Remote Fills	Size, Manifolded	Which tanks?	Suction, Remote, Make if known

8. UNDERGROUND WATER

Depth to the Water table 120+ "

Is the water over the tank? ☐ Yes ☒ No

9. FILL-UP ARRANGEMENTS

Tanks to be filled _____ hr _____ Date Arranged by _____ Name _____ Telephone

Extra product to "top off" and run TSTT How and who to provide? Consider NO Lead.

Terminal or other contact for notice or inquiry _____ Company _____ Name _____ Telephone

10. CONTRACTOR, MECHANICS, any other contractor involved

11. OTHER INFORMATION OR REMARKS

REPAIRED PUMPS

Additional information on any items above. Officials or others to be advised when testing is in progress or completed. Visitors or observers present during test etc.

12. TEST RESULTS

Tests were made on the above tank systems in accordance with test procedures prescribed for petro Tite as detailed on attached test charts with results as follows:

Tank Identification	Tight	Leakage Indicated	Date Tested
#1	TIGHT	+.026	8-2-86
#2	TIGHT	+.039	8-2-86
#3	TIGHT	+.032	9-10-86

13. CERTIFICATION

This is to certify that these tank systems were tested on the date(s) shown. Those indicated as "Tight" met the criteria established by the National Fire Protection Association Pamphlet #329.

ACCURATE TANK TESTING, INC.

14. SUNOL CHEVRON — 8/2/86

Name of Supplier, Owner or Dealer | Address No. and Street(s) | City | State | Date of Test

15. TANK TO TEST

#1

Identity by position

CHEVRON UNLEADED

Brand and Grade

16. CAPACITY

Nominal Capacity 1000 Gallons

By most accurate capacity chart available 1005 Gallons

Is there doubt as to True Capacity? [ ]

See Section "DETERMINING TANK CAPACITY"

From
[X] Station Chart
[ ] Tank Manufacturer's Chart
[ ] Company Engineering Data
[ ] Charts supplied with petro tite
[ ] Other ______

17. FILL-UP FOR TEST

Stick Water Bottom before Fill-up Ø to ⅛ in. ______ Gallons

	Stick Readings to ⅛ in.	Gallons	Total Gallons as Reading
Inventory			1005
Fill up. STICK BEFORE AND AFTER EACH COMPARTMENT DROP OR EACH METERED DELIVERY QUANTITY	TOP OFF		+5
Product in full tank (up to fill pipe)			1010

Tank Diameter PERMANENT SPLASH TUBE

18. SPECIAL CONDITIONS AND PROCEDURES TO TEST THIS TANK

OBS API 60
OBS TEMP 84
CORR API 57

See manual sections applicable. Check below and record procedure in log (28).

[ ] Water in tank [ ] High water table in tank excavation [ ] Line(s) being tested with LVLLT

VAPOR RECOVERY SYSTEM
[ ] Stage I
[ ] Stage II

19. TANK MEASUREMENTS FOR TSTT ASSEMBLY

Bottom of tank to Grade* .... 91½"
Add 30" for 4" ⅊ .... ______"
Add 24" for 3" ⅊ or air seal .... ______"
Total tubing to assemble Approximate .... ______"

20. EXTENSION HOSE SETTING

Tank top to grade* ______"
Extend hose on suction tube 6" or more below tank top ______"

*If Fill pipe extends above grade, use top of fill.

21. TEMPERATURE/VOLUME FACTOR (a) TO TEST THIS TANK

Is Today Warmer? [ ] Colder? [ ] ____°F Product in Tank ____°F Fill-up Product on Truck ____°F Expected Change (+ or −)

22. Thermal-Sensor reading after circulation 16368 digits 72/23 Nearest °F

23. Digits per °F in range of expected change 323 digits

24. 1010 total quantity in full tank (16 or 17) × .00059230 coefficient of expansion for involved product = 0.598223 volume change in this tank per °F gallons

25. 0.598223 volume change per °F (24) ÷ 323 Digits per °F in test Range (23) = .001852 Volume change per digit. Compute to 4 decimal places. This is test factor (a) .0018

28. LOG OF TEST PROCEDURES		29. Reading No.	30. HYDROSTATIC PRESSURE CONTROL — Standpipe Level in Inches: Beginning of Reading	Level to which Restored	31. VOLUME MEASUREMENTS (V) RECORD TO .001 GAL. — 32. Product in Graduate: Before Reading	After Reading	Product Replaced (−) / Product Recovered (+)	34. TEMPERATURE COMPENSATION USE FACTOR (a) — 35. Thermal Sensor Reading	36. Change Higher + Lower − (c)	37. Computation (c) × (a) = Expansion + Contraction −	38. NET VOLUME CHANGES EACH READING — Temperature Adjustment: Volume Minus Expansion (+) or Contraction (−) #33(V) − #37(T)	39. ACCUMULATED CHANGE — At High Level record Total End Deflection; At Low Level compute Change per Hour (NFPA criteria)
Time	Record details of setting up and running test. (Use full length of line if needed.)											

petro tite
HEATH CONSULTANTS
100 TOSCA DRIVE
P.O. BOX CS-200
STOUGHTON, MA 02072-1591
(617) 344-1400

27. Time (24 hr)	28. Record details of setting up and running test. (Use full length of line if needed.)	29. Reading No.	Pressure Control: Standpipe Level in inches — Beginning of Reading	Standpipe Level in inches — Level to which Restored	Volume Measurements (V) Record to .001 gal.: 32. Product in Graduate — Before Reading	Product in Graduate — After Reading	Product Replaced (−) / Product Recovered (+)	Temperature Compensation Use Factor (a): 35. Thermal Sensor Reading	36. Change Higher + Lower − (c)	37. Computation (c) × (a) = Expansion + Contraction −	Changes Each Reading: Temperature Adjustment — Volume Minus Expansion (+) or Contraction (−) #33(V) ÷ #37(T)	Accumulated Change: At High Level record Total Lvl Deflection / At Low Level compute Change per Hour (NFPA criteria)
0910	BEGIN CIRCULATION											
0920	THERMAL SENSOR READING							17021				
0935	START 42" HIGH LEVEL TEST			42		.840		147				
0950		1	44	42	.840	.930	+.090	187	+40	+.072	+.018	
1005		2	44.2	42	.520	.620	+.100	237	+50	+.090	+.010	
1020		3	43.8	42	.620	.710	+.090	289	+52	+.093	−.003	
1035		4	44.4	42	.710	.810	+.100	344	+55	+.099	+.001	
1040	DROP TO LOW LEVEL											
1050	START 12" LOW LEVEL TEST			12		.530		778				
1105		1	14.5	12	.530	.640	+.110	831	+53	+.100	+.010	
1120		2	14.2	12	.640	.740	+.100	889	+48	+.091	+.009	+.039
1135		3	14.5	12	.740	.850	+.110	942	+53	+.100	+.010	
1150		4	14.5	12	.850	.960	+.110	995	+53	+.100	+.010	
	CRITERIA OF ± .050 GALLON/HOUR											
	The criteria established of ± .050											
	gallon/hour is a mathematical											
	calculation based on actual liquid											
	volume change and temperature											
	change, and is not intended as a											
	permission of a leak.											
	DAVID E. COTTLE #414810964											

26. LOG OF TEST PROCEDURES			PRESSURE CONTROL		VOLUME MEASUREMENTS (27) RECORD TO 001 GAL			TEMPERATURE COMPENSATION USE FACTOR (a)			CHANGES EACH READING	
27. DATE / TIME (24 hr.)	28. Record details of setting up and running test. (Use full length of line if needed.)	29. Reading No.	Standpipe Level in Inches: Beginning of Reading	Standpipe Level in Inches: Level to which Restored	32. Product in Graduate: Before Reading	Product in Graduate: After Reading	Product Replaced (−) / Product Recovered (+)	35. Thermal Sensor Reading	36. Change Higher (+) Lower (−) (c)	37. Compensation for Expansion or Contraction	Temperature Adjustment: Volume Minus Expansion (+) or Contraction (−) #33-V − #37(T)	At High Level record Total Leak Reduction / At Low Level compute Change per Hour (EPA criteria)
0955	CIRCULATION PUMP PRIMED AND RUNNING											
1000	FIRST SENSOR READING							16961				
1015	START 42" HIGH LEVEL TEST			42		.620		954				
1030	HIGH LEVEL TEST CONT.	1	42.0	42	.620	.620	+.000	992	+38	+.030	−.030	
1045	" " " "	2	42.0	42	.620	.620	+.000	032	+40	+.032	−.032	
1100	" " " "	3	41.8	42	.620	.610	−.010	068	+36	+.029	−.039	
1115	" " " "	4	41.8	42	.610	.600	−.010	103	+35	+.028	−.038	
1120	DROP TO LOW LEVEL.											
1130	START 12" LOW LEVEL TEST			12		.410		135				
1145	LOW LEVEL TEST CONT	1	12.0	12	.410	.410	+.000	165	+30	+.024	−.024	
1200	" " " "	2	12.2	12	.410	.420	+.010	193	+28	+.022	−.012	−.032
1215	" " " "	3	12.4	12	.420	.440	+.020	219	+26	+.021	−.001	
1230	" " " "	4	12.5	12	.440	.465	+.025	244	+25	+.020	+.005	

CRITERIA OF ± .050 GALLON/HOUR

~~The criteria established of ± .050~~ gallon/hour is a mathematical calculation based on actual liquid ~~volume change and temperature~~ change, and is not intended as a permission of a leak.

DAVID E. COTTLE #414810964