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### SELF-MONITORING REPORT – FOURTH QUARTER & YEAR 2006 NPDES PERMIT NO. CAG912002

GROUNDWATER REMEDIATION AT CITY OF OAKLAND MUNICIPAL SERVICES CENTER 7101 EDGEWATER DRIVE OAKLAND, CALIFORNIA

Prepared for

City of Oakland Public Works Agency Environmental Services Division 250 Frank H. Ogawa Plaza, Suite 5301 Oakland, CA94612

January 2007

Prepared by

**OTG** Enviroengineering Solutions, Inc.

464 19<sup>th</sup> Street, Suite 206 Oakland, CA 94612

### OTG EnviroEngineering Solutions, Inc.

January 15, 2007

Mr. Farhad Azimzadeh Regional Water Quality Control Board 1515 Clay Street, Suite 1400 Oakland, CA 94612

Reference: RWQCB Order No. 01-100, NPDES Permit #CAG912002

Subject: Self-Monitoring Report – Fourth Quarter and Year 2006 Groundwater Remediation at 7101 Edgewater Drive, Oakland, CA

Dear Mr. Azimzadeh:

On behalf of the City of Oakland, OTG Enviroengineering Solutions, Inc. is pleased to submit this Self-Monitoring Report for a groundwater extraction, treatment and discharge system at the City of Oakland Municipal Services Center (MSC) located at 7101 Edgewater Drive, Oakland, California. No violations of RWQCB Order No. 01-100 and NPDES Permit #CAG912002 were identified during this reporting period of time.

#### Certification

I certify under penalty of law that this document and all attachments are prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gathered and evaluated the information submitted. Based on my inquiry of the person or persons who managed the system, or those persons directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations.

Please contact the undersigned at (510) 465-8982 if you have questions or comments.

Sincerely, OTG EnviroEngineering Solutions, Inc.

Xinggang Tong, PhD, PE Project Manager



cc: Mr. Gopal Nair, City of Oakland Mr. Barney Chan, Alameda County Department of Environmental Health

464 19<sup>th</sup> Street, Suite 206, Oakland, CA 94612 (510) 465-8982, fax (510) 868-0667 Mailing Address: P.O. Box 70125, Oakland, CA 94612

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### TABLE OF CONTENTS

SEC	CTION	Page
1.	INTRODUCTION	1
2.	DESCRIPTION OF REMEDIATION SYSTEM	2
3.	OPERATIONS AND MAINTENANCE	2
4.	DISCHARGE MONITORING – FOURTH QUARTER AND YEAR 2006	3
5.	REFERENCES	5

#### FIGURES

1.	Site Location and Discharge Location	Map
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- 2. Identification of Free-Phase Petroleum Product Locations
- 3. Identification of Extraction Wells and Trench Layout
- 4. Remediation System Process & Instrumentation Diagram
- 5. Schematic of Groundwater Treatment System and Sampling Locations

#### **TABLES**

- 1 Summary of Laboratory Analytical Procedures
- 2 Summary of Operational Data and Field Measured Parameters
- 3 Summary of Petroleum Hydrocarbon Analytical Data
- 4 Summary of Analytical Data for Inorganic Constituents and Fish Bioassay
- 5 Summary of Analytical Data for Organic Constituents
- 6 TPH Removed Through Dissolved Phase and Floating Product

#### **APPENDICES**

A. Laboratory Analytical Reports for Fourth Quarter, 2006 Samples

### **1** INTRODUCTION

The City of Oakland Municipal Services Center (MSC) is located at 7101 Edgewater Drive, Oakland, CA (Figure 1). The site was originally part of a waterfront tidal marsh complex, which was filled between 1950 and 1971. The MSC occupies an area of approximately 17 acres. The City leased the land from the Port of Oakland for use as a corporation yard. Bordering the MSC site to the west and the north is the Martin Luther King Regional Shoreline Park. This park land is also owned by the Port of Oakland. Damon Slough is located to the north, and commercial developments are located to the east and south.

The MSC site has been the subject of numerous environmental investigations starting in about 1989. The suspected sources of on-site contamination include releases from underground storage tanks (USTs), gasoline and diesel fuel hydrant system, and the floor drain waste collection pits formerly located adjacent to Building No. 5. In addition, some or all of the material used to fill the site may have been waste or contaminated prior to placement at the site. A comprehensive investigation conducted by Baseline in 2000 identified the existence of freephase petroleum hydrocarbon product at four separate areas within the MSC. They are labeled as Plumes A through D on Figure 2. Baseline's investigation is documented in the report of *Site History and Characterization* (January 2001).

Groundwater monitoring has been conducted quarterly from the fourth Quarter of 1989 through the third quarter of 2002 and then semi-annually to current. Shallow groundwater elevation varies from 2 to 10 feet below ground surface and is partially subject to tidal influence. Shallow groundwater flow is toward the southwest to the nearest shoreline along San Leandro Bay across much of the site. In the northern portion of the MSC, groundwater flows in a more northerly direction toward the curving shoreline and Damon Slough (Baseline, January 2001)

Pilot-scale Dual-Phase Extraction (DPE) tests were conducted in 2002 to enhance the removal of free-phase petroleum product from the four identified areas (Cambria, August 13, 2002 and URS, August 29, 2002). Extracted groundwater was treated on-site through two 2,000-lb granular activated carbon units connected in series and discharged to on-site storm drain via a NPDES permit granted by the San Francisco Bay Regional Water Quality Control Board (NPDES Permit No. CAG912002). Based on the pilot test result, the City retained Cambria in May 2003 to design a full-scale application of product recovery and groundwater/soil vapor extraction at Plumes C and D. Cambria's design was revised in October 2005 by Groundwater and Environmental Services (GES) to focus the first phase of product removal in Plume D. The final design drawings were included in Appendix A of the Startup Report (OTG, June 2006). Chemical oxidation and enhanced bioremediation through periodic injections of hydrogen peroxide have been implemented in Plumes A, B and C since July 2004.

In March 2006, the City retained URS Corporation and its subcontractor ERRG to construct the GES' revised remediation system of product recovery and groundwater/soil vapor extraction. The construction was completed in early May 2006. On May 22, 2006, the product recovery and groundwater extraction portion of the remediation system was turned on.



### 2. DESCRIPTION OF REMEDIATION SYSTEM

The remediation system consists of extraction of liquid (petroleum product and groundwater) and soil vapor from seven (7) wells located in Plume D area (Figure 3), separation of petroleum product from groundwater, treatment of groundwater by activated carbon, discharge of treated water to local storm drain via a NPDES permit, treatment of soil vapor, and discharge of treated vapor to the atmosphere via an air discharge permit. A process and instrumentation diagram of the remediation system is illustrated on Figure 4. Design details were included in Appendix A of the Startup Report (OTG, June 2006).

The seven wells are: RW-D1, RW-D2, RW-D3, RW-D4, RW-D5, TBW-5 and RW-1. Their locations are shown on Figure 3. RW-D1 through RW-D5 were constructed in December 2001 specifically for remediation purposes, and RW-1 and TBW-5 were placed during backfilling of the excavation of former fuel hydrant lines in the early 1990s. Each well is equipped with a total fluid recovery pneumatic pump specifically designed for viscous petroleum product recovery. The pump is manufactured by Clean Environment Equipment in Oakland and has the Model # AP-Custom. An Ingersoll-Rand air compressor (model # SSR UP6-10) provides compressed air to the pneumatic pumps. Each well is also piped into a high vacuum extraction unit that can produce up to 28 inches of mercury vacuum. This vacuum unit can be operated at either mode of soil vapor extraction only or soil vapor and liquid simultaneous extraction. The pneumatic pumps and the vacuum extraction unit can be operated independently.

The liquid extracted by the pneumatic pumps and the vacuum unit is pumped into an oil/water separator (Model # AGM-3SS-90V, Hydro Quip, Inc.). Recovered oil is contained in 55-gallon drums, which are sent to an off-site oil recycling facility. Groundwater is treated through three (3) granular activated carbon (GAC) units connected in series (Model #ASC-2000, U.S.Filter/Westates Carbons) before been discharged into local storm drain. Each GAC unit contains 2,000 lbs of GAC. Figure 5 illustrates the groundwater treatment portion of the remediation system and identifies sampling ports.

A 40 hp liquid-ring vacuum pump capable of 500 ACFM and up to 28" Hg extracts soil vapor and liquid from the seven wells. The vapor is abated by a combination of thermal and catalytic oxidizer. At low vapor organic concentrations, activated carbon can also be used for vapor abatement.

### **3 OPERATIONS AND MAINTENANCE**

On May 22, 2006, the pneumatic pumps were turned on to start the remediation process. The vacuum extraction portion remained off line. Because the free-phase product appears to be a mixture of gasoline, diesel, and some other highly viscous organics (petroleum tank bottom or coal tar like material), the vacuum extraction, if turned on, will vaporize gasoline and a portion of the diesel and will make the removal of the viscous product even more difficult. The plan is to first use the pneumatic pumps to remove the free-phase product as much as practically achievable and then to use the vacuum extraction system to enhance the removal of the remaining petroleum hydrocarbons.



The groundwater extraction, treatment, and discharge system was operated continuously during the Fourth Quarter 2006. Operations and maintenance (O&M) of the system were performed following the instruction of *Operation &Maintenance Manual for Groundwater Remediation System at City of Oakland Municipal Services Center, Draft* (OTG, July 2006), which included daily check of air compressor's oil & pressure levels, functions of liquid level sensors and pumps, draining condensate from air tank, removing oil from the oil/water separator, and other tasks necessary for maintaining proper functions of the remediation system. No carbon changes were performed this quarter since no chemical breakthrough was detected in any of the three carbon vessels.

On-site measurement included temperature, pH, and electric conductivity using an Oakton pH/Con 10 meter (Serial #311648) and turbidity using an Oakton T-100 meter (Serial #316738). Before measurement, the pH probe was calibrated with standard solutions of pH 4.00, 7.00, and 10.00; the electric conductivity probe calibrated with 1413 ug/cm standard solution; and the turbidity meter calibrated with standards of 0.02, 20.0, 100, and 800 NTUs.

Chemical analyses were performed by Curtis & Tompkins, Ltd of Berkeley. Fish toxicity bioassay was conducted by Block Environmental Services of Pleasant Hill. The data received from laboratories was found to be of acceptable quality with qualifications as noted in the laboratory reports.

### 4 DISCHARGE MONITORING – FOURTH QUARTER AND YEAR 2006

Field measured data and laboratory analysis results are summarized in the following tables:

- Table 1 Summary of Laboratory Analytical Procedures
- Table 2 Summary of Operational Data and Field Measured Parameters
- Table 3 Summary of Petroleum Hydrocarbon Analytical Data
- Table 4 Summary of Analytical Data for Inorganic Constituents & Fish Bioassay
- Table 5 Summary of Analytical Data for Organic Constituents
- Table 6 TPH removed through Dissolved in Groundwater and Floating Product

#### Major highlights for the Fourth Quarter 2006 are:

- Liquid extraction by the seven pneumatic pumps ran continuously for this reporting period (October 1 through December 31, 2006). A total of 168,460 gallons of groundwater was extracted within the plume D area, treated, and discharged into the local storm drain, resulting in an average monthly flow rate of 1.69 gallons per minute (gpm) in October, 1.07 gpm in November, and 1.07 gpm in December.
- 70 gallons of separate-phase floating product was recovered. Counting the TPH removed with the groundwater (dissolved phase), approximately 80 gallons, or 568 lbs, of TPH was removed.



- Monthly monitoring was conducted on October 4, November 8, and December 6. Monthly monitoring results are summarized in Tables 2 and 3. Quarterly monitoring was conducted on November 8 and results are presented in Tables 4 and 5.
- Effluent (treated groundwater) had pHs between 7.1 and 7.35, temperatures between 12.3 and 19.4 °C, conductivities between 10.03 and 15.4 ms/cm, and turbidities between 0.04 and 0.1.
- TPH gas, diesel, benzene, toluene, ethylbenzene, and xylenes (BTEX), and MTBE in the monthly effluent samples were all below their respective reporting limits.
- Daily mass discharges calculated based on the average daily flow rate and the quarterly monitoring data (November 8) for all inorganic constituents were significantly below their respective daily mass limits imposed by the discharge permit for the category of less than 10 gpm discharge rate (Table 4).
- The rainbow trout survival rate was 100% in the 96-hour static renewal bioassay conducted for the effluent sample collected on November 8 (Table 4).
- The average concentration for the influent (after the oil/water separator, but before the carbon treatment) for the Fourth Quarter 2006 was 43 mg/L TPH gas, 8.2 mg/L TPH diesel, and 4.67 mg/L benzene.

### Major highlights for Year 2006 are:

- A total of 547,431 gallons of groundwater was extracted from May 22, when the groundwater extraction and treatment system was turned on, through December 31, 2006, resulting in an average flow rate of 1.70 gpm.
- 315 gallons of separate-phase floating product was recovered. Counting the TPH removed with the groundwater (dissolved phase), approximately 352 gallons, or 2,490 lbs of TPH was removed.
- Effluent (treated groundwater) had pHs between 6.95 and 8.3, temperatures between 12.3 and 23.6 °C, conductivities between 8.81 and 15.4 ms/cm, and turbidities between 0.04 and 0.2.
- TPH gas, diesel, benzene, toluene, ethylbenzene, and xylenes (BTEX), and MTBE in the monthly effluent samples were all below their respective discharge limits at all times.
- Daily mass discharges calculated based on the average daily flow rate and the quarterly monitoring data for all inorganic constituents were significantly below their respective daily mass limits imposed by the discharge permit for the category of less than 10 gpm discharge rate.
- The rainbow trout survival rate was 100% in the 96-hour static renewal bioassay conducted quarterly for the effluent.
- Effluent concentrations of volatile organic compounds (VOCs) and fuel oxygenates analyzed by EPA8260 and semi-VOCs analyzed by EPA8270 and EPA8310 were all below their respective reporting limits.
- Influent groundwater (after the oil/water separator, but before carbon treatment) had TPH gas concentrations of between 32 and 60 mg/L, TPH diesel between 4.0 and 25 mg/L, and benzene between 3.1 and 6.1 mg/L.



#### **5 REFERENCES**

Baseline Environmental Consulting, Site History and Characterization, January 2001

Cambria Environmental Technology, Inc. *TPE Pilot Test and Feasibility Report*, August 13, 2002.

California Regional Water Quality Control Board – San Francisco Bay Region, Authorization to Discharge Treated Groundwater Under the Requirements of Order No. 01-100, NPDES Permit No. CAG 912002, April 23, 2002.

OTG Enviroengineering Solutions, Inc. Self-Monitoring Report – Third Quarter 2006, Groundwater Remediation at City of Oakland Municipal Services Center, October 2006

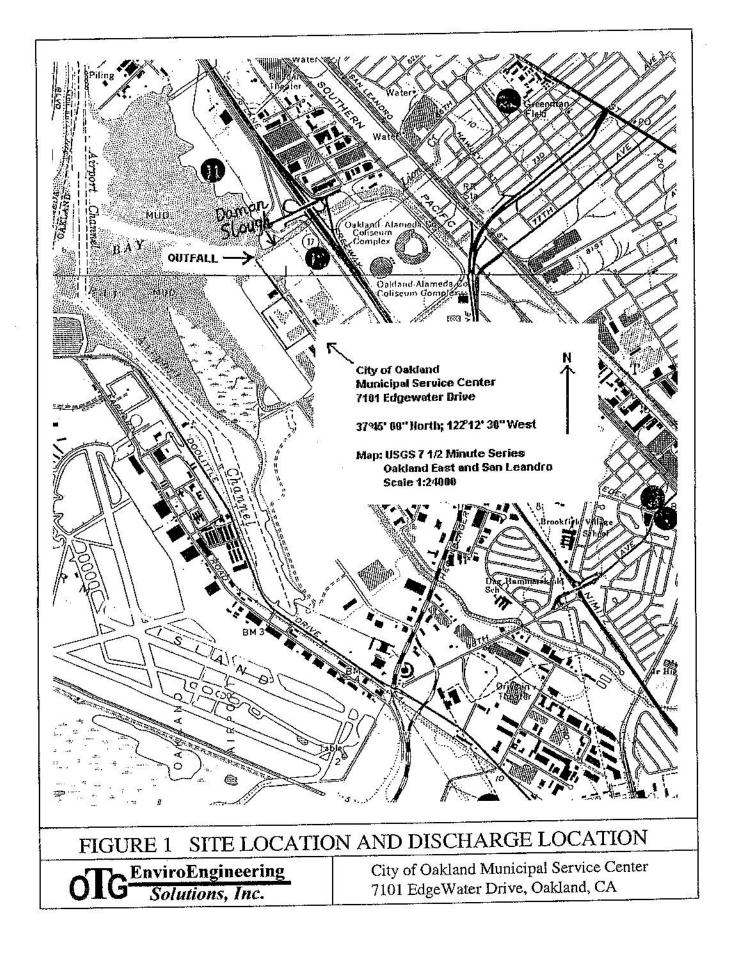
OTG Enviroengineering Solutions, Inc. Self-Monitoring Report – Second Quarter 2006, Groundwater Remediation at City of Oakland Municipal Services Center, July 2006

OTG Enviroengineering Solutions, Inc. Operation & Maintenance Manual for Groundwater Remediation System at City of Oakland Municipal Services Center, Draft, July 2006

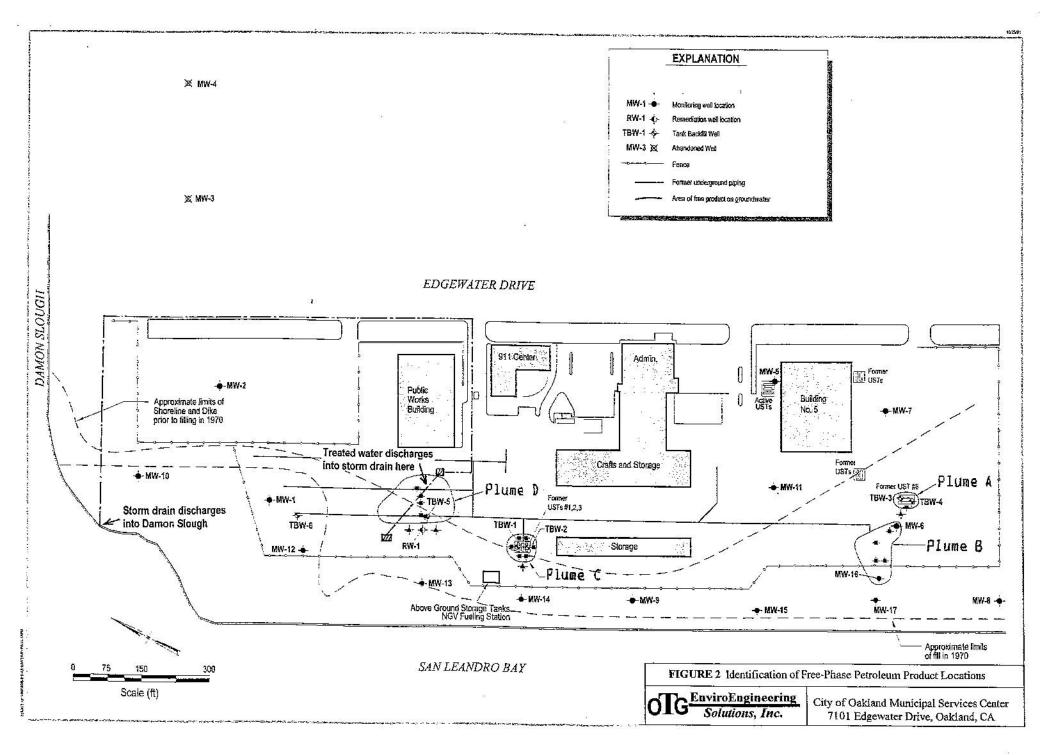
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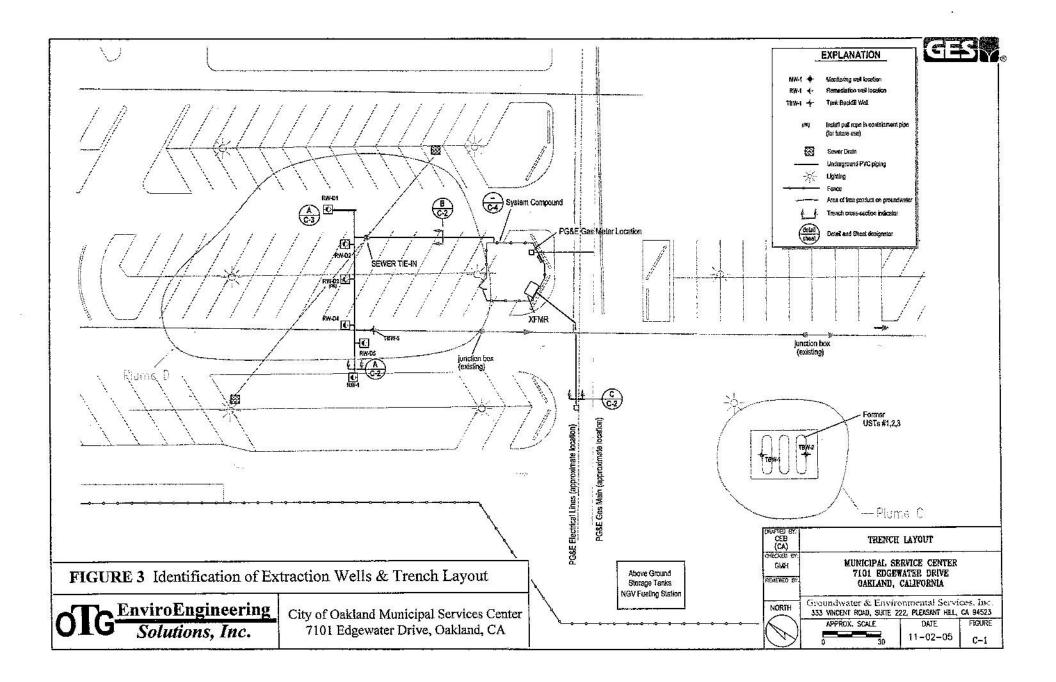
URS Corporation, *Results of Dual-Phase Extraction Pilot Test for Plumes A & B, City of Oakland Municipal Services Center*, August 29, 2002.



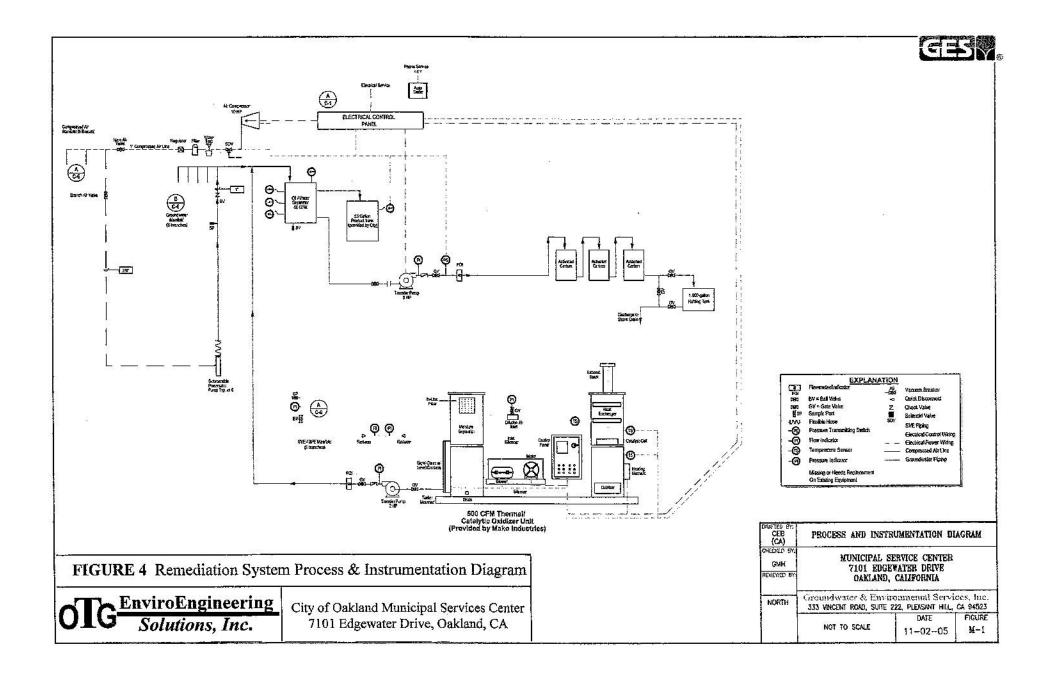


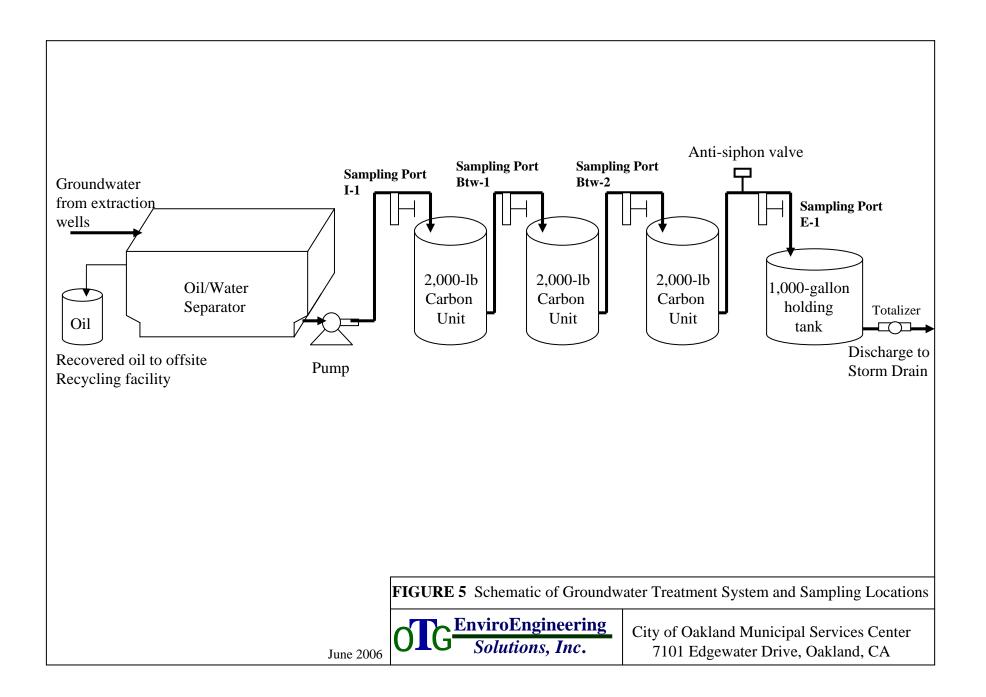
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## **Table 1** - Summary of Laboratory Analytical Procedures City of Oakland Municipal Services Center Groundwater Remediation Project

	5/22/06	5/30/06	6/26/06	7/25/06	9/5/06	10/4/06	11/8/06
	0/22/00	0/00/00	0/20/00	& 8/11/06	0/0/00	& 12/6/06	11/0/00
Flow rate	onsite totalizer	onsite totalizer	onsite totalizer		onsite totalizer		onsite totalizer
Turbidity	on-site	on-site	on-site	on-site	on-site	on-site	on-site
Fish bioassay			EPA/821/R-02/012		EPA/821/R-02/0		EPA/821/R-02/012
pH	on-site	on-site	on-site	on-site	on-site	on-site	on-site
DO				on one			
	on-site	on-site	on-site	on-site	on-site	on-site	on-site
E. conductivity		on-site	on-site	on-site	on-site	on-site	on-site
L. conductivity							
Benzene	EPA 8021B	EPA 8021B	EPA 8021B	EPA 8021B	EPA 8260B	EPA 8021B	EPA 8021B
Toluene	EPA 8021B	EPA 8021B	EPA 8021B		EPA 8260B	EPA 8021B	EPA 8021B
Ethylbenzene		EPA 8021B	EPA 8021B		EPA 8260B		
	EPA 8021B	EPA 8021B	EPA 8021B		EPA 8260B	EPA 8021B	EPA 8021B
MTBE	EPA 8021B	EPA 8021B	EPA 8021B		EPA 8260B	EPA 8021B	
TPH g&d	EPA 8015B	EPA 8015B	EPA 8015B		EPA 8015B	EPA 8015B	
EDB		EPA 8260B			EPA 8260B		
VOCs		EPA 8260B			EPA 8260B		
TAME		EPA 8260B			EPA 8260B		
DIPE		EPA 8260B			EPA 8260B		
ETBE		EPA 8260B			EPA 8260B		
ТВА		EPA 8260B			EPA 8260B		
Ethanol		EPA 8015B			EPA 8260B		
Methanol		EPA 8015B			EPA 8015B		
SVOCs		EPA 625			EPA 8270C		
PAHs		EPA 610			EPA 8310		
Hardness	SM 2340B	SM 2340B	SM 2340B		SM 2340B		SM 2340B
Antimony	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Arsenic	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Beryllium	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Cadmium	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Chromium	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Cr +6	EPA 7196	EPA 7196	EPA 7199		EPA 7199		EPA 7199
Copper	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Cyanide	EPA 335.2	EPA 335.2	EPA 335.2		EPA 335.2		EPA 335.2
Lead	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Mercury	EPA 245.1	EPA 245.1	EPA 7470A		EPA 7470A		EPA 7470A
Nickel	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Selenium	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Silver	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Thallium	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
Zinc	EPA 200.8	EPA 200.8	EPA 6020		EPA 6020		EPA 6020
n 1/0 or duet 't	/Tomptours				actor Carlat //O	14040	
pH/Conductivit calibrated daily		neasured on-si	e using a Oakton	рп/Con 10 n	neter, Serial #31	11048,	
		to using a Oakt	on T-100 meter, S	orial #31673	8 calibrated da	ily before use	<u> </u>
rubulty was f	neasureu on-Si	te using a Oakl	un i-iuu metel, S	benai #310/3	o, calibrateu da	ily belore use	

Date	Time			uent (E-1)			nfluent		Btw-1	Btw-2	Totalizer	Monthly	Monthly	Product	Notes
		рΗ		E. conduc	Turbidity	pН		E. cond.			Reading	Treated		recovere	
			(°C)	(ms/cm)	(NTU)		(°C)	(ms/cm)			(gallons)	(gallons)	(gal/min)	(gallons)	
5/22/2006											1,389				Before turn on system
5/22/2006	11:25	8.3	20.4	8.81	0.2	7.12	21.4	10.2	sampled		2,050				treated water held in tank
5/22/2006	14:15										2,414				stopped, waiting for analy data
5/24/2006	13:00										2,414				system on, start discharge
5/30/2006	12:30	7.48	19.4	8.25	0.04	6.98	23.1	8.32	sampled		14,230			20	
5/31/2006	10:00										18,980	17,591	1.705		
6/2/2006	16:30								sampled	sampled	31,080				
6/9/2006	8:30										48,610				
6/16/2006	10:20										67,755				
6/19/2006	9:40										74,670				
6/22/2006	11:00										90,480				
6/26/2006	9:00	7.32	22.3	13	0.1	7.37	23.3	13.4	sampled	sampled	106,950				Monthly monitoring
6/30/2006	9:00										122,860	103,880	2.405	100	
7/5/2006	10:00										140,500				two full drums of product
7/12/2006	9:30								sampled	sampled	163,230				
7/19/2006	9:30								· · ·		182,740				
7/25/2006	9:30	7.35	23.6	12.5	0.04	7.4	24.2	13.1	sampled		197,030				Monthly monitoring
7/31/2006	19:30										212,010	89,150	1.997	155	
8/2/2006	19:30										216,790			165	three full drums of product
8/9/2006	9:00										233,260				Morgan removed 3 drums prodt
8/11/2006	9:30	6.95	21.5	12.8	0.1	7.25	22.3	12.6	sampled	sampled	238,380				Monthly monitoring
8/14/2006	8:00										246,180				lowered pumps in wells
8/17/2006	11:30										255,030				
8/28/2006	11:30										283,080				
9/1/2006	18:30										294,910		1.801	220	one full drum of product
9/5/2006		7	19.7	12.3	0.1	7.1	22.8	11.5	sampled	sampled					Monthly & Qtrly monitoring
9/9/2006	18:00										310,750				
9/17/2006											333,310				
9/22/2006	13:30										349,210				
9/27/2006											364,350				
9/29/2006											371,290				
10/2/2006											380,360		1.925	245	
10/4/2006		7.1	19.4	12.67	0.04	7.3	21.5	12.22	sampled	sampled					monthly monitoring
10/9/2006											402,090				
10/16/2006											417,310				
10/23/2006											436,170				
10/27/2006											443,640				
10/30/2006	11:00										448,220			275	two full drums of product

## **Table 2** - Summary of Operational Data and Field Measured Parameters City of Oakland Municipal Services Center Groundwater Remediation Project

Date	Time		Efflu	uent (E-1)		li	nfluent	(I-1)	Btw-1	Btw-2	Totalizer	Monthly	Monthly	Product	Notes
		pН	Tempt	E. conduc	Turbidity	pН	Tempt	E. cond.			Reading	Treated	ave. rate	recovere	d
			(°C)	(ms/cm)	(NTU)		(°C)	(ms/cm)			(gallons)	(gallons)	(gal/min)	(gallons)	
11/1/2006	10:30										453,340	72,980	1.689		
11/8/2006	11:00	7.35	18.6	10.03	0.1	7.03	21.7	10.79	sampled	sampled	461,210				monthly & quarterly monitoring
11/14/2006	12:30										483,660				
11/20/2006	10:30										487,970				
12/1/2006	11:30										499,540	46,200	1.069	295	
12/6/2006	11:00	7.1	12.3	15.4	0.08	8.45	14.8	17.7	sampled	sampled	504,500				monthly monitoring
12/15/2006	10:00										513,050				
12/22/2006	14:30										533,130				
12/27/2006	10:00										540,340			315	2 full drums plus 40 gal product
1/2/2007	9:00										548,820	49,280	1.073		

## **Table 2** - Summary of Operational Data and Field Measured Parameters City of Oakland Municipal Services Center Groundwater Remediation Project

Date	Effluent (E-1)       Influent (I         TPH gas       TPHdiesel       benzene       toluene       ethyl benz       xylenes       MTBE       TPH gas       TPHdiesel       benzene       toluene         (ug/L)       (ug/L)	nfluent (I-1	)											
1	TPH gas	TPHdiesel	benzene	toluene	ethyl benz	xylenes	MTBE	TPH gas	TPHdiesel	benzene	toluene	ethyl benz	xylenes	MTBE
	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)
Eff. Limit	50						_							
5/22/2006	( )	. ,	ND (0.5)	· · /	. ,		ND (2.0)		25,000 (h,l)	6,100		1,200		ND (100)
5/30/2006	ND (50)	130 (y, a1)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	57,000	9,200 (l,y)	4900	5300	1100	7100	ND (36)
6/2/2006		ND (50)												
6/26/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	50,000	10,000(h,l,y)	4800	6900	1100	7200	ND (50)
7/25/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	60,000	4,000(l,y)	5800	8800	1100	9000	ND (80)
8/11/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)		4.6 (a1a)	59,000	4,100 (l,y)	4900	7300	930	7000	ND (100)
9/5/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	44,000	4,800 (l,y)	4700	4800	1200	5400	ND (50)
10/4/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	42,000	9,100 (h,l,y)	5100	7300	1400	6700	ND (100)
11/8/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	32,000	7,800 (h,l,y)	3100	3800	590	2880	ND (50)
12/6/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	55,000	7,600 (h,l,y)	5800	8600	820	6600	ND (50)
(a1) - false p					mples at E-	1, Btw-1 & I	Stw-2	(a1a) - fals	e positive, co	nfirmed NI	D on 9/5/06	sample		
(h) - heavier	,													
(I) - lighter hy														
(y) - sample	exhibits ch	romatograp	hic pattern	which does	not resemb	ole standarc								

## **Table 3** - Summary of Petroleum Hydrocarbon Analytical Data City of Oakland Municipal Services Center Groundwater Remediation Project

Date	TPH gas         TPHdiesel         benzene         toluene         ethyl benz         xylenes         MTBE         TPH gas         TPHdiesel         benzene         toluene         ethyl benz         xylenes           (ug/L)         (ug/L)													
	TPH gas	TPHdiesel	benzene	toluene	ethyl benz	xylenes	MTBE	TPH gas	TPHdiesel	benzene	toluene	ethyl benz	xylenes	MTBE
	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)	(ug/L)
Eff. Limit	50	50	5	5	5	5	13	50	50	5		5 5	5	13
					_									
	() /		· · /	· · /	. ,	. ,	. ,							
	( )	ND (50)	. ,	. ,				NA	ND (50)					
	( )	. ,	( )	, ,					. ,	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)
	( )		, ,	, ,				. ,			· · ·	, ,	ND (0.5)	3.9 (a2)
7/25/2006	. ,	. ,	ND (0.5)	, ,	ND (0.5)	ND (0.5)	2.7							
8/11/2006	ND (50)		ND (0.5)		ND (0.5)		5.1 (a2a)	ND (50)	NA	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	5.4 (a2a)
9/5/2006		. ,	ND (0.5)	, ,	ND (0.5)	ND (0.5)			NA	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)
10/4/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	ND (50)	NA	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)
11/8/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	ND (50)	NA	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)
12/6/2006	ND (50)	ND (50)	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)	ND (50)	NA	ND (0.5)	ND (0.5)	ND (0.5)	ND (0.5)	ND (2.0)
(a2) - false	positive det	tection, cont	firmed ND a	after the firs	t carbon un	it	(a2a) - fals	e positive d	letection, co	onfirmed ND	on 9/5/06	sample		
(h) - heavie	r hydrocarb	ons contrib	uted to the	quantitation	1									
(I) - lighter h	nydrocarboi	ns contribut	ed to the qu	antitation										
(y) - sample	e exhibits cl	nromatograp	phic pattern	which does	s not resem	ble standar	d							

## **Table 3** - Summary of Petroleum Hydrocarbon Analytical Data City of Oakland Municipal Services Center Groundwater Remediation Project

Constituen	nUnit	Eff Limit	Effluer	nt (E-1)						
	(	<10 gpm)	5/22/06	5/30/06	6/26/06	9/5/06	11/8/06			
Antimony	ug/L		2.3	1.8	0.12	0.13	0.35			
, i	g/day	3	0.02137	0.01672	0.001572	0.00138	0.00243			
Arsenic	ug/L		36			3	4.3			
	g/day	1	0.33444	0.22296	0.0917	0.03177	0.0298			
Beryllium	ug/L		ND (0.35)	ND (0.5)	ND (0.055)	ND (0.12)	ND (0.12)			
	g/day	3								
Cadmium	ug/L		1	0.5	ND (0.14)	ND (0.17)	ND (0.17)			
	g/day	1	0.00929	0.00465						
Total Cr	ug/L		3.1	ND (0.5)	0.62	0.86	0.78			
	g/day	2	0.0288		0.008122	0.00911	0.00541			
Cr +6	ug/L		ND (1.0)	ND (10)	ND (0.5)	ND (0.5)	ND (0.5)			
	g/day	2								
Copper	ug/L		1.3	0.9	1.3	1.5	1.2			
	g/day	3	0.01208	0.00836	0.01703	0.01589	0.00832			
Lead	ug/L		ND (0.1)	ND (0.25)	0.26	0.3	0.3			
	g/day	5			0.003406	0.00318	0.00208			
Mercury	ug/L		ND(0.008)	ND(0.2)	ND (0.2)	ND (0.06)	ND (0.02)			
	g/day	0.01								
Nickel	ug/L		11	67	15	9.6	2.9			
	g/day	5	0.10219	0.62243	0.1965	0.10166	0.0201			
Selinium	ug/L		3			ND (0.35)	1.2			
	g/day	2	0.02787				0.00832			
Silver	ug/L		ND (0.02)	ND (0.1)	ND (0.041)	ND (0.07)	ND (0.07)			
	g/day	1								
Thallium	ug/L			ND (0.1)		ND (0.03)	ND (0.03)			
	g/day	3	0.00056		0.002751					
Zinc	ug/L			ND (10)	44	11	1.9			
	g/day	10	0.01858		0.5764					
Cyanide	ug/L		ND (0.8)	ND (3)	ND (10)	ND (10)	ND (10)			
	g/day									
	mg/LCaCO3		560	960	1100	1100	1,500			
Fish Bioa										
% surviva	al of Rainbow	/ Trout			100%	100%	100%			

## **Table 4** - Summary of Analytical Data for Inorganic Constituents and Fish Bioassay City of Oakland Municipal Services Center Groundwater Remediation Project

Inorganic	Unit	Eff Limit	Influe	nt (I-1)					
		(<10 gpm)	5/22/06	5/30/06	11/8/	)6			
Antimony	ug/L		ND (60)	ND (1)					
	g/day	3	()	( )					
Arsenic	ug/L		7.2	8.5					
	g/day	1		0.07897					
Beryllium	ug/L			ND (1)					
	g/day	3		. ,					
Cadmium	ug/L		34	10					
	g/day	1	0.31586	0.0929					
Total Cr	ug/L		ND (10)	ND (1)					
	g/day	2							
Cr +6	ug/L		ND (0.5)	ND (0.5)					
	g/day	2							
Copper	ug/L		250	25					
	g/day	3	2.3225	0.23225					
Lead	ug/L		28	21					
	g/day	5	0.26012	0.19509					
Mercury	ug/L		ND (0.2)	ND (0.2)					
	g/day	0.01							
Nickel	ug/L		68						
	g/day	5		0.17651					
Selinium	ug/L			ND (1)					
	g/day	2	0.08733						
Silver	ug/L		ND (5)	ND (1)					
	g/day	1							
Thallium	ug/L			ND (1)					
	g/day	3	0.23225						
Zinc	ug/L		31	57					
	g/day	10	0.28799						
Cyanide	ug/L		10			20			
	g/day		0.0929	0.0929					

## **Table 4** - Summary of Analytical Data for Inorganic Constituents and Fish Bioassay City of Oakland Municipal Services Center Groundwater Remediation Project

		Effluent (E	-1)				
			,				
	Max Daily	5/30/06	9/5/06				
	Eff. Limit	0,00,00	0,0,00				
	(ug/L)	(ug/L)	(ug/L)				
Benzene	<u>(ag</u> , <u>_</u> ) 5		ND (0.5)				
Carbon tetrachloride	5		ND (0.5)				
Chloroform	5		ND (0.5)				
1,1-Dichloroethane	5		ND (0.5)				
1,2-Dichloroethane	5		ND (0.5)				
1,1-dichloroethylene	5		ND (0.5)				
Ethylbenzene	5		ND (0.5)				
Methylene chloride	5		ND (0.5)				
Tetrachloroethylene	5		ND (0.5)				
Toluene	5		ND (0.5)				
c-1,2-Dichloroethylene	5		ND (0.5)				
t-1,2-Dichloroethylene	5		ND (0.5)				
1,1,1-Trichloroethane	5		ND (0.5)				
1,1,2-Trichloroethane	5		ND (0.5)				
Trichloroethylene	5		ND (0.5)				
vinyl chloride	5		ND (0.5)				
total xylenes	5		ND (0.5)				
MTBE	13		ND (0.5)				
Ethylene dibromide	5		ND (0.5)				
Trichlorotrifluoroethane	5		ND (5)				
TPH gas	50		ND (50)				
TPH diesel	50		ND (50)				
		(00)					
TAME		ND (0.5)	ND (0.5)				
DIPE			ND (0.5)				
ETBE			ND (0.5)				
ТВА			ND (10)				
Ethanol		ND(1000)					
Methanol		ND(1000)	ND(1000)				
Other VOCs (EPA 8260)		ND	ND				
PAHs (EPA 8310 or 610)							
All analytes		ND (1.0)	ND (0.1)				
, ·		( -/	<u>\ /</u>				
SVOCs(EPA8270 or625)							
All analytes		ND (5.0)	ND (9.4)				
		(0.0)	()				
L					I	1	1

	Influent (I-1	)			
	5/30/06	/			
Deserve	(ug/L)				
Benzene	4900				
Carbon tetrachloride	ND (36)				
Chloroform	ND (36)				
1,1-Dichloroethane	ND (36)				
1,2-Dichloroethane	ND (36)				
1,1-dichloroethylene	ND (36)				
Ethylbenzene	1100				
Methylene chloride	ND (36)				
Tetrachloroethylene	ND (36)				
Toluene	5300				
c-1,2-Dichloroethylene	ND (36)				
t-1,2-Dichloroethylene	ND (36)				
1,1,1-Trichloroethane	ND (36)				
1,1,2-Trichloroethane	ND (36)				
Trichloroethylene	ND (36)				
vinyl chloride	ND (36)				
total xylenes	7100				
MTBE	ND (36)				
Ethylene dibromide	ND (36)				
Trichlorotrifluoroethane	ND (360)				
TPH gas	57000				
TPH diesel	9200				
TAME	ND (36)				
DIPE	ND (36)				
ETBE	ND (36)				
ТВА	ND (710)				
Ethanol	ND(1000)				
Methanol	ND(1000)				
Other VOCs (EPA 8260)	110(1000)				
Isopropylbenzene	40				
Propylbenzene	120				
1,3,5-Trimethylbenzene	410				
1,2,4-Trimethylbenzene	1500				
Naphthalene	370				
Naphinalene	370				
PAHs (EPA 8310 or 610)	4 7				
Benzo(a)anthracene	1.7				
Benzo(a)pyrene	1.6				
Chrysene	2.6				
Fluoranthene	3.8				
Naphthalene	130				
Pyrene	3.3				
SVOCs(EPA8270 or625)					
Dimethylphthalate	28				
bis(2-Ethylhexyl)phthalate	12				
Naphthalene	290				
Phenol	13				
	1	l	1	1	·

r		After Eirot	Carbon Unit (Daur	()			<b>1</b>
		After First	Carbon Unit (Btw-1	1)			
	Mary Daily	E /00/00	0/5/00				
	Max Daily	5/30/06	9/5/06				
	Eff. Limit	(					
	(ug/L)	(ug/L)					
Benzene	5	ND (0.5)	ND (0.5)				
Carbon tetrachloride	5	ND (0.5)	NA				
Chloroform	5	ND (0.5)	NA				
1,1-Dichloroethane	5	ND (0.5)	NA				
1,2-Dichloroethane	5	ND (0.5)	NA				
1,1-dichloroethylene	5	ND (0.5)	NA				
Ethylbenzene	5	ND (0.5)	ND (0.5)				
Methylene chloride	5	ND (0.5)	NA				
Tetrachloroethylene	5	( )	NA				
Toluene	5		ND (0.5)				
c-1,2-Dichloroethylene	5	ND (0.5)	NA				
t-1,2-Dichloroethylene	5	ND (0.5)	NA				
1,1,1-Trichloroethane	5	ND (0.5)	NA				
1,1,2-Trichloroethane	5	ND (0.5)	NA				
Trichloroethylene	5		NA				
vinyl chloride	5		NA				
total xylenes	5		ND (0.5)				
MTBE	13	ND (0.5)	ND (2)				
Ethylene dibromide	5	ND (0.5)	NA				
Trichlorotrifluoroethane	5		NA				
TPH gas	50		ND (50)				
TPH diesel	50	ND (50)	ND (50)				
TAME		ND (0.5)	NA				
DIPE		ND (0.5)	NA				
ETBE		ND (0.5)	NA				
ТВА		ND (10)	NA				
Ethanol		NA	NA				
Methanol		NA	NA				
Other VOCs (EPA 8260)		ND	NA				
PAHs (EPA 8310 or 610)		NA					
SVOCs(EPA8270 or625)		NA					
		1		1	1	1	1

		After Second Carbon		
	Max Daily	9/5/06		
	Eff. Limit			
	(ug/L)	(ug/L)		
Benzene	5	ND (0.5)		
Carbon tetrachloride	5	ND (0.5)		
Chloroform	5	ND (0.5)		
1,1-Dichloroethane	5	ND (0.5)		
1,2-Dichloroethane	5	ND (0.5)		
1,1-dichloroethylene	5	ND (0.5)		
Ethylbenzene	5	ND (0.5)		
Methylene chloride	5	ND (0.5)		
Tetrachloroethylene	5	ND (0.5)		
Toluene	5	ND (0.5)		
c-1,2-Dichloroethylene	5	ND (0.5)		
t-1,2-Dichloroethylene	5	ND (0.5)		
1,1,1-Trichloroethane	5	ND (0.5)		
1,1,2-Trichloroethane	5	ND (0.5)		
Trichloroethylene	5	ND (0.5)		
vinyl chloride	5	ND (0.5)		
total xylenes	5	ND (0.5)		
MTBE	13	ND (0.5)		
Ethylene dibromide	5	ND (0.5)		
Trichlorotrifluoroethane	5	ND (5)		
TPH gas	50	NA		
TPH diesel	50	NA		
TAME		ND (0.5)		
DIPE		ND (0.5)		
ETBE		ND (0.5)		
ТВА		ND (10)		
Ethanol		ND (1000)		
Methanol		NA		
Other VOCs (EPA 8260)		ND		
`,				
PAHs (EPA 8310 or 610)		NA		
,				
SVOCs(EPA8270 or625)		NA		

Month	groundwater	TPH gas	TPH diesel	Mass remov	ed through gro	oundwater	Floating produ	total monthly	/ % removed	Cumulative pro	duct removed
	removed	Influent	Influent	as TPH gas	s TPH gas as TPH diesel co		recovered	removal	by floating	(Floating + Dissolved)	
	(gallons)	(mg/L)	(mg/L)	(lbs)	(lbs)	(lbs)	(gallons)	(gallons)	product	(gallons)	(lbs)
May-06	17,591	54.5	17.1	7.98	2.50	10.49	20	21.48	0.93	21.48	152
Jun-06	103,880	50	10	43.25	8.65	51.90	80	87.33	0.92	108.81	770
Jul-06	89,150	60	4	44.54	2.97	47.51	65	71.71	0.91	180.53	1278
Aug-06	82,900	59	4.1	40.73	2.83	43.56	55	61.15	0.90	241.68	1711
Sep-06	85,450	44	4.8	31.31	3.42	34.72	25	29.91	0.84	271.59	1922
Oct-06	72,980	42	9.1	25.52	5.53	31.05	30	34.39	0.87	305.97	2166
Nov-06	46,200	32	7.8	12.31	3.00	15.31	20	22.16	0.90	328.14	2323
Dec-06	49,280	55	7.6	22.57	3.12	25.69	20	23.63	0.85	351.77	2490
Jan-07											
Note:	Morgan dispo	osed of 3 5	5-gallon dru	ums full of rec	overed produc	t on 8/9/06					

# **Table 6** - TPH Removed Through Dissolved in Groundwater and Floating Product City of Oakland Municipal Services Center Groundwater Remediation Project

### **APPENDIX** A

Laboratory Analytical Reports for Fourth Quarter 2006 Samples

