



Chevron U.S.A. Products Company

2410 Camino Ramon, San Ramon, California • Phone (510) 842-9500
Mail Address: PO Box 5004, San Ramon, CA 94583-0804

93 APR 26 1993

April 26, 1993

Ms. Jennifer Eberle
Alameda County Health Care Services
80 Swan Way, Room 200
Oakland, CA 94621

478

**Re: Former Chevron Service Station #9-4816
301 14th Street, Oakland**

Dear Ms. Eberle:

Enclosed we are forwarding the Bimonthly Progress Report dated April 19, 1993, prepared by our consultant Weiss Associates for the above referenced site. This report presents an evaluation of the soil vapor extraction and treatment system operating at the referenced site during the period of February 1, 1993 to March 31, 1993. During this period approximately 517 lbs. of hydrocarbons were removed. Cumulative to date, approximately 10,961 lbs. of hydrocarbons (approximately 1,660.75 gallons) have been recovered. The system was down between the periods of February 24th through March 15th for servicing of the ICE engine printer and March 24th through March 29th due to a lack of propane. An additional well northeast of the treatment enclosure was installed on March 31, 1993, to increase the effectiveness in this area.

which? VEW-3.
See 4-30-93 G-T report

Chevron will continue to submit bimonthly progress reports on the soil vapor extraction system until system shutdown. We plan to replace the ICE Engine with vapor-phase carbon within the next month. The ICE Engine is no longer cost effective based on the influent concentrations.

If you have any questions or comments, please do not hesitate to contact me at (510) 842-9581.

Very truly yours,
CHEVRON U.S.A. PRODUCTS COMPANY


Nancy Vukelich
Site Assessment and Remediation Engineer

Enclosure

cc: Mr. Rich Hiatt, RWQCB
Mr. R.W. Cosby, 225/1936
Ms B.C. Owen
File (9-4816-8)

Ms. Beth D. Castleberry
Ware & Freidenrich
400 Hamilton Avenue
Palo Alto, CA 94301-1825



April 19, 1993

Nancy Vukelich
Chevron U.S.A. Products Company
P.O. Box 5004
San Ramon CA 94583-0804

Re: Bi-monthly Progress Report
February through March 1993
Chevron Service Station #9-4816
301-14th Street
Oakland, California
WA Job #4-582-52

Dear Ms. Vukelich,

As you requested, Weiss Associates (WA) presents the following bi-monthly report for the soil vapor extraction (SVE) and treatment system operating at the above-referenced site (Figure 1). The SVE and treatment system consists of an internal combustion engine (ICE) which presently extracts vapors from wells VEW-1, VEW-2 and CR-1 (Figure 2). ICE operation is permitted by the Bay Area Air Quality Management District (BAAQMD) under Permit to Operate #8272. The system operated in compliance throughout this reporting period.

In accordance with BAAQMD requirements, WA monitors the influent and effluent vapor stream monthly. Samples are collected in Tedlar bags for submittal to a state-certified analytical laboratory where they are analyzed for total petroleum hydrocarbons as gasoline (TPH-G), benzene, ethylbenzene, toluene and total xylenes. Additionally, field measurements are taken with a flame ionization detector (FID) or photo ionization detector (PID). Table 1 presents a summary of analytic results, FID/PID measurements, hours of system operation, calculated emission rates and estimated destruction efficiencies since system start-up. Table 2 presents calculated hydrocarbon removal rates and total pounds of hydrocarbons removed. Figure 3 illustrates total pounds of hydrocarbons removed from the site via SVE and hydrocarbon removal rate versus time. We estimate that as of March 18, 1993, about 10,961 lbs (1,661 gallons) of hydrocarbons have been removed from soil and ground water beneath the site. As shown on Figures 4 and 5, influent concentrations have declined from 100,000 parts per million by volume (ppmv) to 160 ppmv since mid-March 1992. Benzene concentrations have declined from 1,800 to 1.3 ppmv. The analytical reports and chain-of-custody forms for

February and March 1993 are included as Attachment A. A sample emissions calculation based on the BAAQMD Manual of Procedures for Soil Vapor Extraction dated July 12, 1991, is presented as Attachment B.

The SVE system was down between February 24 and March 15 for ICE printer servicing and system upgrade. Because the ICE is designed to shut down if the printer is disconnected, we were unable to operate the engine while the printer was being repaired and cleaned. WA used the system down time to install a new, larger oil reservoir which reduces the need for frequent engine oil changes.

The system also shut down on February 1 and between March 24 to 29 due to a lack of propane. Because of influent hydrocarbon concentration fluctuations during this period, propane usage has been erratic and unpredictable. WA currently schedules propane deliveries for twice per week to help ensure that the system operates on a continual basis.

In conjunction with vapor stream monitoring, WA measured separate-phase hydrocarbon thicknesses in onsite wells. These measurements are presented in Table 3. During February and March, separate-phase hydrocarbons were not detected in any onsite wells. Separate-phase hydrocarbons have not been detected in any onsite wells since January 11, 1993.

Hydrocarbon mass removal rates were 5.3 and 1.0 lbs/day in February and March, respectively. We therefore recommend replacing the ICE with more cost-effective carbon for vapor treatment.

Nancy Vukelich
April 19, 1993

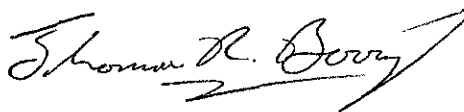
3

As required, WA will continue monthly monitoring and bimonthly reporting. Please call if you have any questions or require additional information.

Sincerely,
Weiss Associates



Kimberly Ohara
Staff Engineer



Thomas R. Berry, R.G.
Project Geologist

TRB:kao

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- Attachments:
- Figure 1 - Site Location Map
 - Figure 2 - Monitoring and Extraction Well Locations
 - Figure 3 - Total Hydrocarbon Removal
 - Figure 4 - Influent Concentrations
 - Figure 5 - Influent Concentrations
 - Table 1 - System Performance and Analytic Results
 - Table 2 - Total Hydrocarbon Removal
 - Table 3 - Free Product Thickness
 - Attachment A - Analytical Reports and Chain-of-Custody Forms
 - Attachment B - Sample Emission Calculations

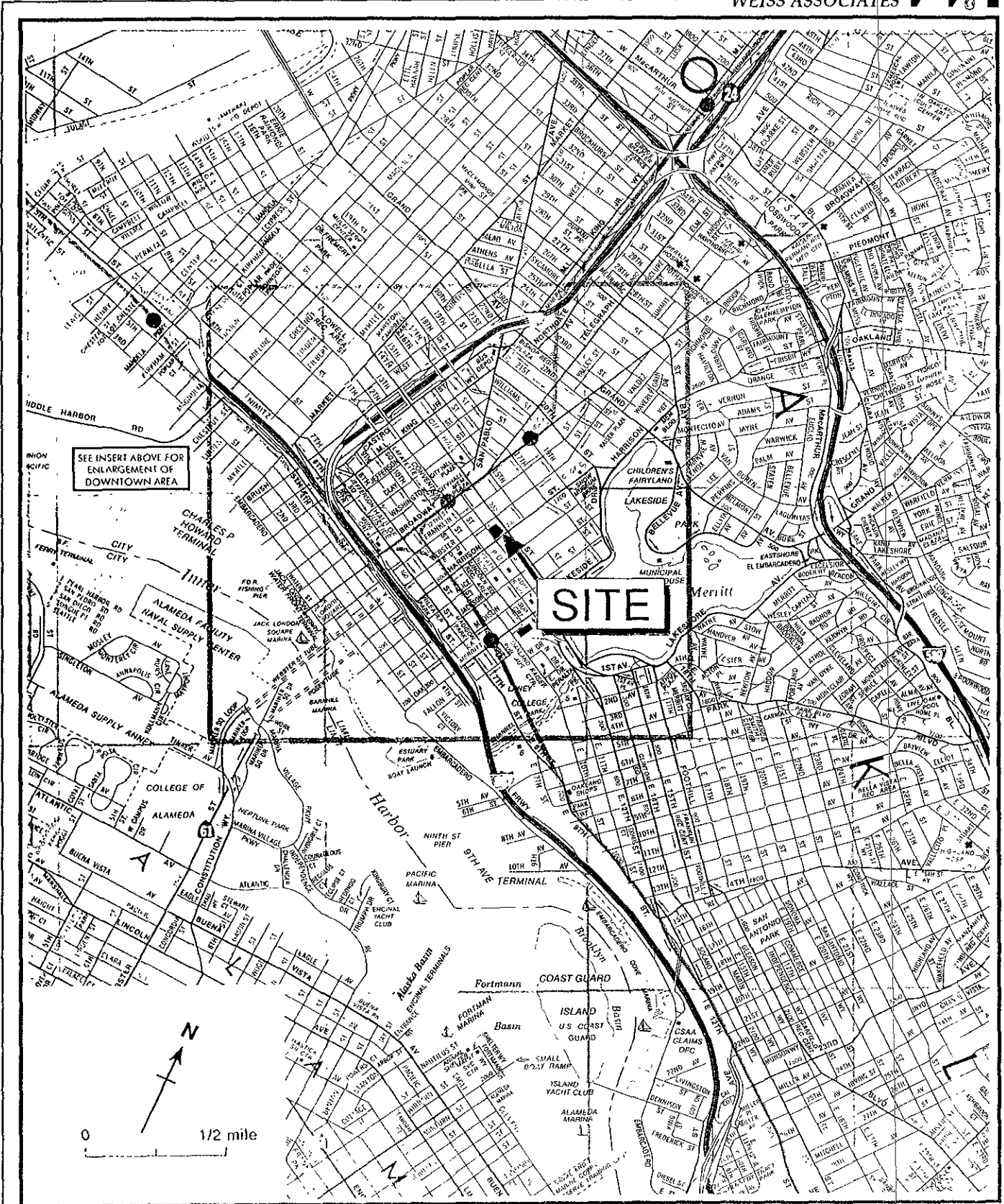


Figure 1. Site Location Map - Former Chevron Service Station #9-4816, 301 14th Street, Oakland, California

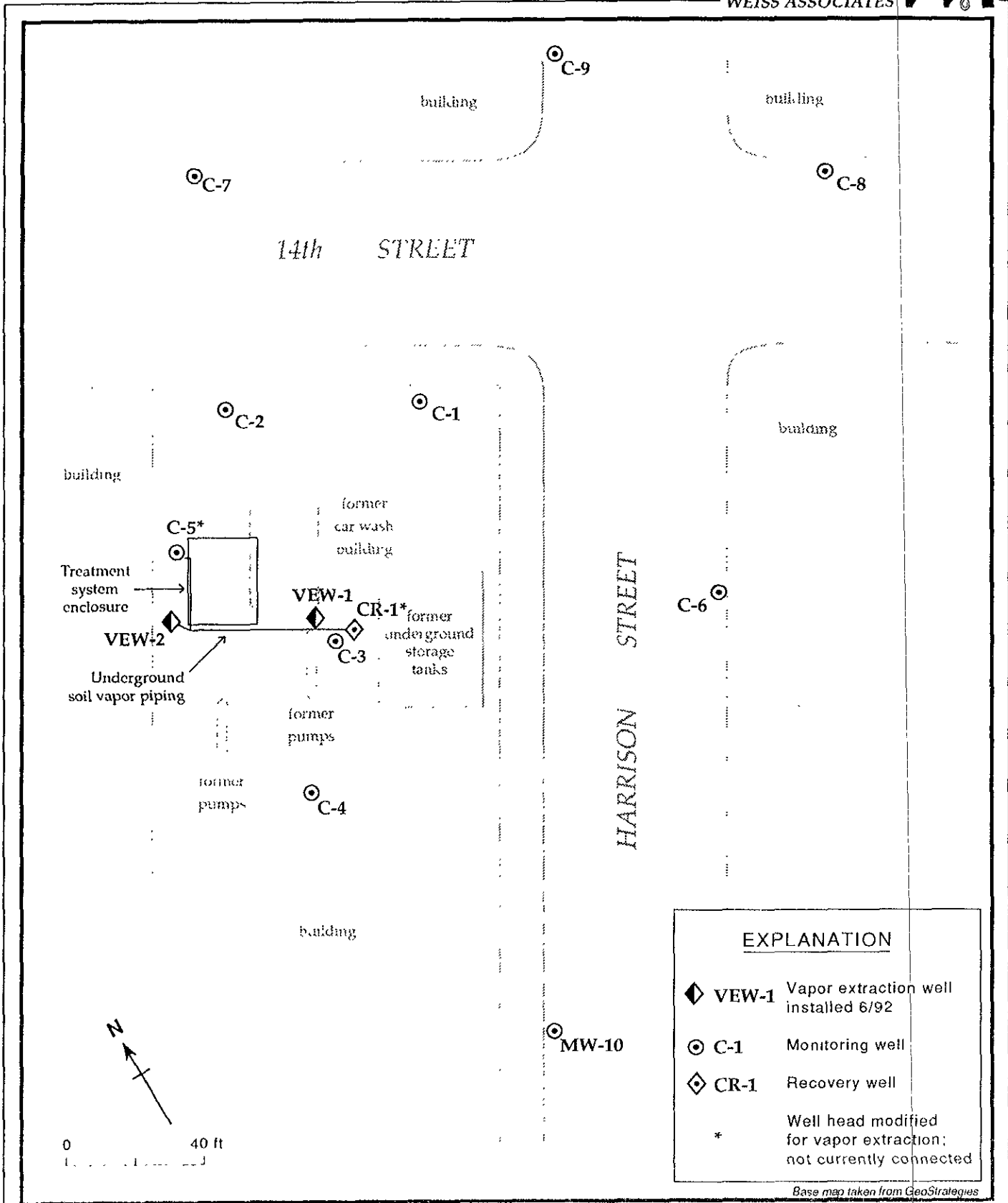
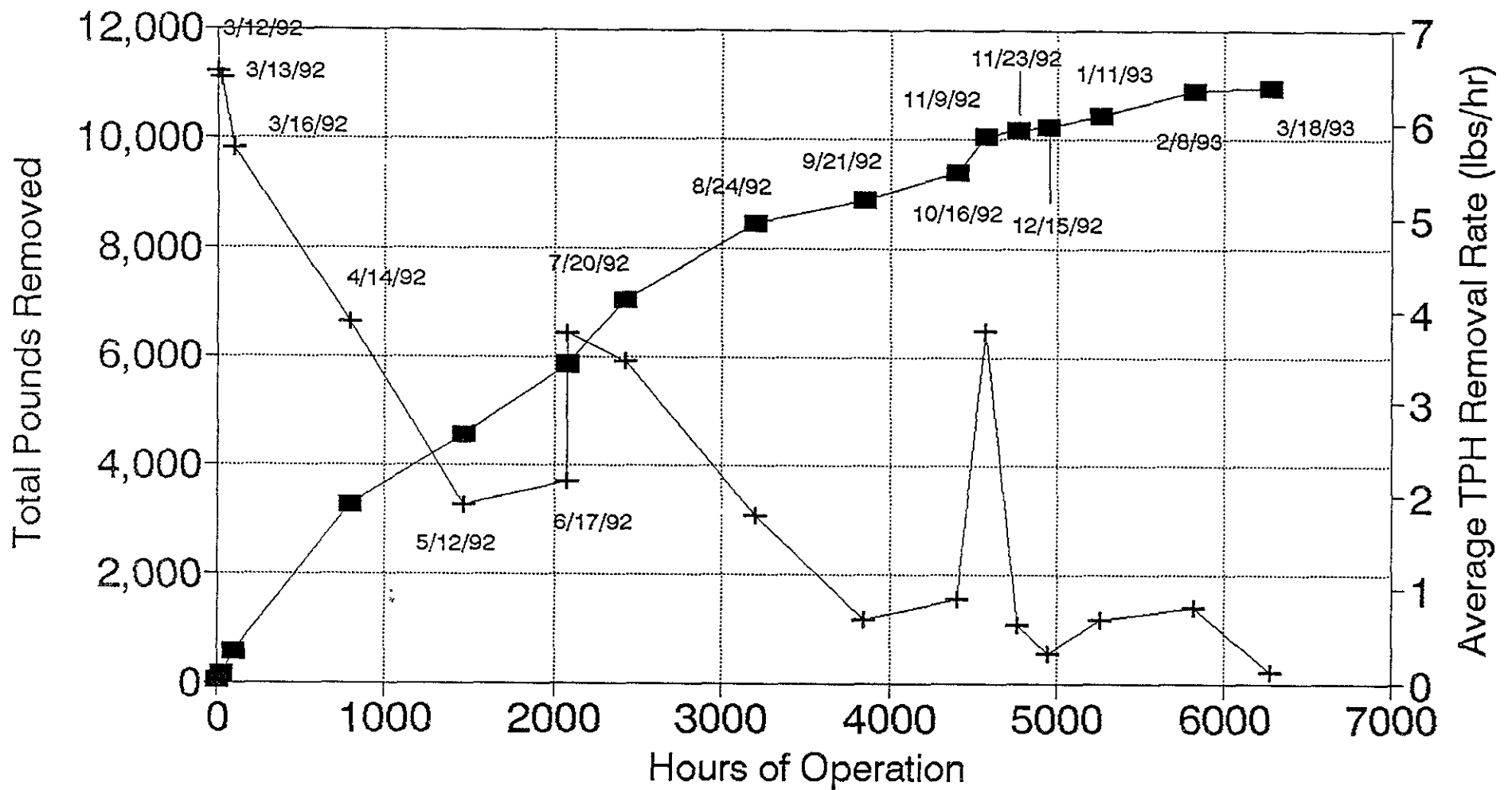


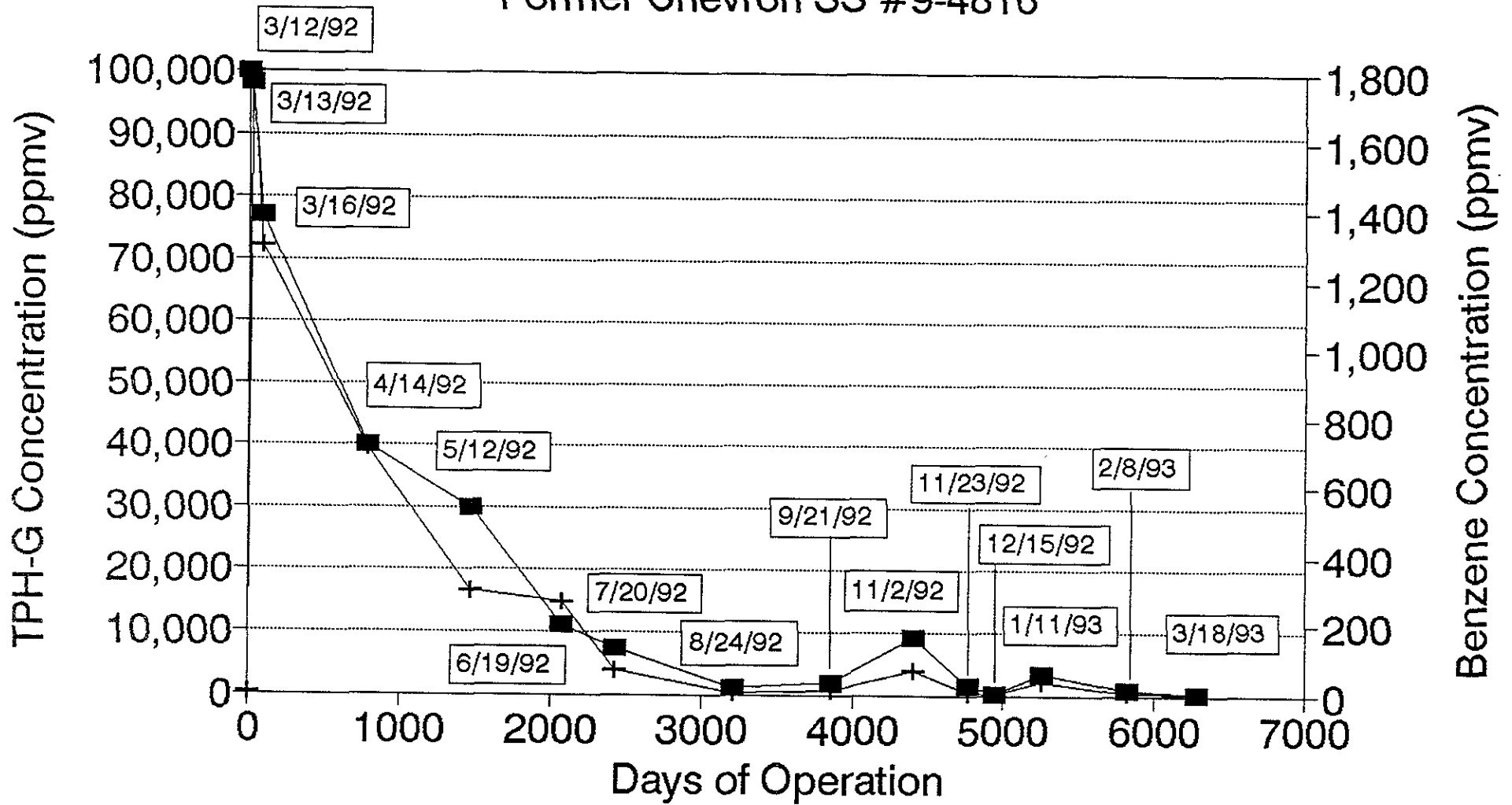
Figure 2. Monitoring and Extraction Well Locations - Former Chevron Service Station #9-4816, 301 14th Street, Oakland, California

Figure 3. Total Hydrocarbon Removal
Former Chevron SS#9-4816, Oakland



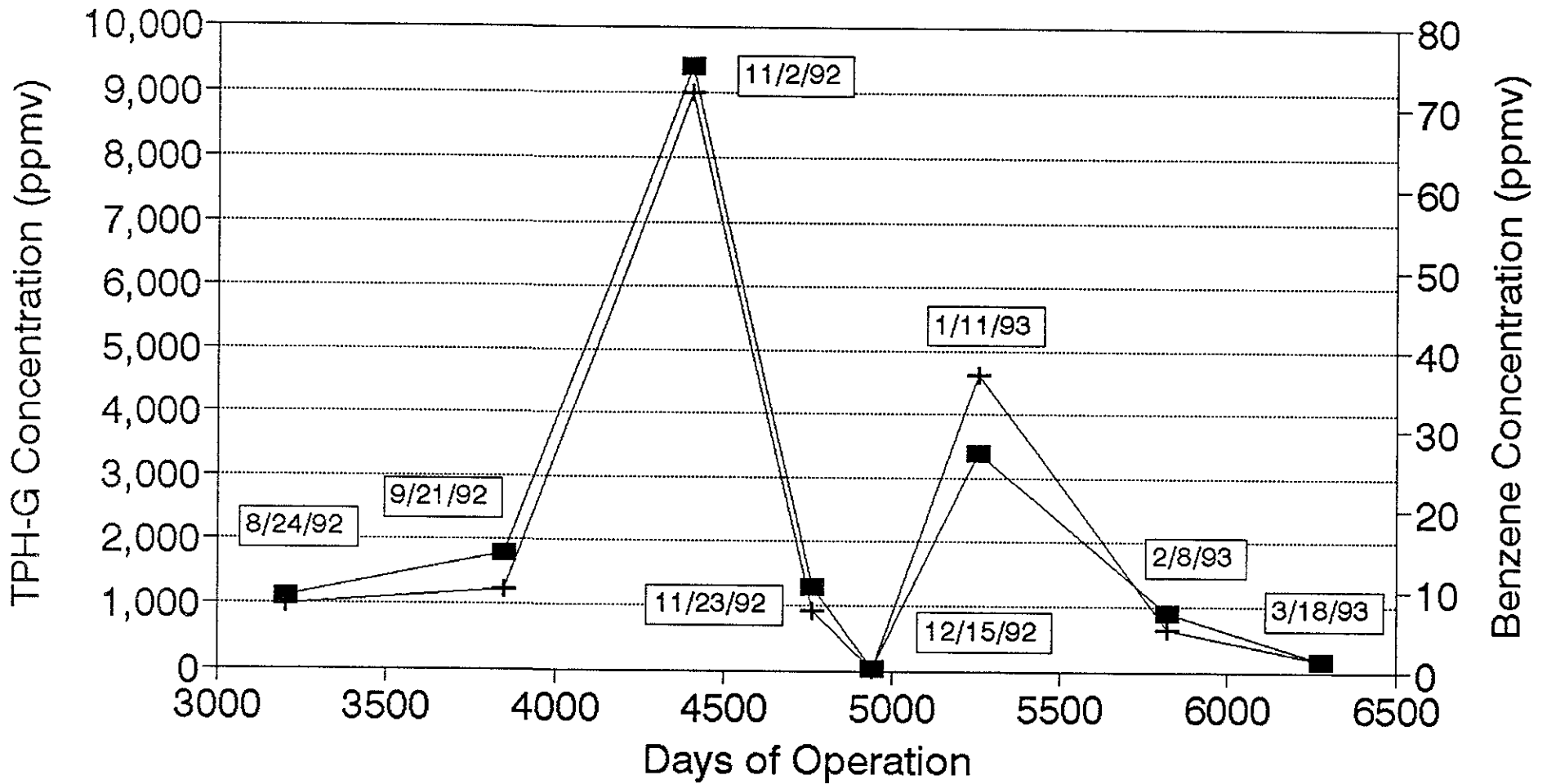
—■— Total lbs Removed —+— Avg. Removal Rate

Figure 4. Influent Concentrations
Former Chevron SS #9-4816



—■— TPH-G (ppmv) —+— Benzene (ppmv)

Figure 5. Influent Concentrations
Former Chevron SS #9-4816



TPH-G (ppmv)

 Benzene (ppmv)



Table 1. System Performance and Analytic Results, Former Chevron SS#9-4816, 301 14th Street, Oakland, California

Date	Well ID a	Total Hours b	Total Well Gas Flow Rate (scfm)		Total System Flow Rate (scfm)	Fuel Hydrocarbon Concentrations (ppmv)						
						FID c	Influent TPH-G	B	FID c	Effluent TPH-G	B	
03/12/92	CR-1/C-5	5	4.9	f	34.5	>46,000	100,000	<4.2	185	<30	<0.085	
03/13/92	CR-1/C-5	23	4.9	f	27.0	>47,800	98,000	1,800	80	<30	<0.085	
03/16/92	CR-1/C-5	98	4.9	f	26.5	>50,000	77,000	1,300	NA	<30	0.12	
04/14/92	CR-1/C-5	790	5.1	h	39.3	2,550	40,000	710	NA	<30	0.54	
05/12/92	CR-1/C-5	1,465	2.7	h	52.9	6,500	30,000	300	NA	450	8.1	
05/26/92	CR-1/C-5					2,934	---	---	1.9	---	---	
06/17/92	CR-1/C-5	2,071	8.0	h,i	35.1	---	---	---	---	---	---	
06/19/92	CR-1/C-5/VEW1/VEW-2	2,077	25.6	h,m	77.0	2,100	11,000	270	100	<30	0.64	
07/20/92	CR-1/C-5/VEW1/VEW-2	2,422	31.0	h	72.0	900	7,600	70	22	31	0.33	
08/10/92	CR-1/C-5/VEW1/VEW-2	2,700	31.2	h	70.7	750	---	---	---	---	---	
08/10/92	VEW-1/VEW-2	n	34.8	h		1,980	---	---	---	---	---	
08/17/92	VEW-1/VEW-2	3,036	24.7	h	74.1	1,778	---	---	300	---	---	
08/24/92	VEW-1/VEW-2	3,204	31.4	h	67.6	---	1,100	7.8	---	<30	0.15	
08/31/92	VEW-1/VEW-2	3,345			76.2	8,850	---	---	100	---	---	
09/08/92	VEW-1/VEW-2	3,541	38.3	h	78.8	8,760	---	---	100	---	---	
09/21/92	VEW-1/VEW-2	3,852	37.6	h	78.5	15,740	1,800	10	640	<30	<0.085	
11/02/92	VEW-1/VEW-2	4,400	30.2	h	63.0	1,330	9,400	72	100	<30	<0.085	
11/23/92	VEW-1/VEW-2	4,764	35.5	h	74.3	450	1,300	7.5	78	<30	<0.085	
12/07/92	VEW-1/VEW-2	4,941	28.7	h	72.9	10,942	---	---	---	---	---	
12/15/92	VEW-1/VEW-2	4,942	33.0	h	72.8	---	<30	<0.085	---	<30	<0.085	
12/28/92	VEW-1/VEW-2	5,085	17.4	h		1,175	---	---	7.5	---	---	
01/11/93	VEW-1/VEW-2/CR1	q	5,255	30.0	r,s	65.6	t	3,400	37	8.7	<30	0.32
01/18/93	VEW-1/VEW-2/CR1		5,347			42.5	t	---	---	---	---	---
01/25/93	VEW-1/VEW-2/CR1		5,512			40.3	345	---	---	---	---	---
02/02/93	VEW-1/VEW-2/CR1		5,676				351	---	---	---	---	---
02/08/93	VEW-1/VEW-2/CR1		5,818	18.0	r, s	56.4	251	920	5.2	22.1	<30	0.36
03/15/93	VEW-1/VEW-2/CR1		6,214				380	---	---	7	---	---
03/18/93	VEW-1/VEW-2/CR1		6,280	20.1	h	57.8	200	160	1.3	50	<30	0.72

-- Table 1 continues on next page --



Table 1. System Performance and Analytic Results, Former Chevron SS#9-4816, 301 14th Street, Oakland, California

Date	Well ID a	Removal Rate (#/day) d		Emission Rate (#/day) e		Destruction Efficiency (%)				
		TPH-G	B	TPH-G	B	TPH-G	B			
03/13/92	CR-1/C-5	157	<0.06	<0.33	<0.0009	>99.80	g	>85.80	g	
03/16/92	CR-1/C-5	154	2.6	<0.26	<0.0006	>99.80	g	>99.98	g	
04/14/92	CR-1/C-5	121	1.9	<0.26	0.0009	>99.80	g	99.95		
05/12/92	CR-1/C-5	65	1.1	<0.38	0.0062	>99.40	g	99.40		
05/26/92	CR-1/C-5	26	0.24	7.1	0.12	72.60		50.00	i, j	
06/17/92	CR-1/C-5					99.93	k			
06/19/92	CR-1/C-5/VEW1/VEW-2									
07/20/92	CR-1/C-5/VEW1/VEW-2	90	2.0	<0.74	0.014	99.20		99.30		
08/10/92	CR-1/C-5/VEW1/VEW-2	76	0.63	0.72	0.0069	99.00		98.90		
08/10/92	VEW-1/VEW-2	n								
08/17/92	VEW-1/VEW-2									
08/24/92	VEW-1/VEW-2									
08/31/92	VEW-1/VEW-2	11	0.071	<0.65	0.0030	>94.1	g	95.80		
09/08/92	VEW-1/VEW-2					98.9				
09/21/92	VEW-1/VEW-2					98.9				
11/02/92	VEW-1/VEW-2	22	0.11	<0.76	<0.0019	>96.5	g	>98.3	g	
11/23/92	VEW-1/VEW-2	91	0.63	<0.61	<0.0016	>99.3	g	>99.7	g	
12/07/92	VEW-1/VEW-2	15	0.077	<0.72	<0.0018	>95.1	g	>97.7	g	
12/15/92	VEW-1/VEW-2									
12/28/92	VEW-1/VEW-2	<0.32	<0.00082	<0.70	<0.0018	u		u		
01/11/93	VEW-1/VEW-2/CR1	q	33	0.32	<0.56	0.0054	>99.0	g	98.3	g
01/18/93	VEW-1/VEW-2/CR1								g	
01/25/93	VEW-1/VEW-2/CR1								g	
02/02/93	VEW-1/VEW-2/CR1									
02/08/93	VEW-1/VEW-2/CR1	5.3	0.027	<0.48	0.0052	>90.9		80.7		
03/15/93	VEW-1/VEW-2/CR1									
03/18/93	VEW-1/VEW-2/CR1	1.0	0.0076	<0.42	v	>58.0	g	v		

-- Table 1 continues on next page --



Table 1. System Performance and Analytic Results, Former Chevron SS#9-4816, 301 14th Street, Oakland, California

Notes:

- a = Measurements/samples represent combined extraction from wells listed.
- b = Total hours of operation equals engine hours as they appear on engine computer printout minus 3050 hours of previous use at other sites.
- c = Value reflects subtraction of carbon-tip (methane) measurement. In some cases, FID measurement of total VOCs exceeded instrument measurement range of 50,000 p
- d = Removal rate based on total well gas flow rate.
- e = Emission rate based on total system flow rate which includes system dilution air and is measured by the ICE internal flow sensor.
- f = Based on flow data for similar operation parameters, measured vacuum, and assumed influent temperature of 70 F.
- g = Destruction efficiency calculation limited by analytic detection limit.
- h = Based on measured vacuum and flow, and assumed influent temperature of 70 F.
- i = System was shut down May 19, 1992, immediately following receipt of analytic results indicating system non-compliance due to low system destruction efficiency. Low efficiency was due to system adjustments made during a manufacturer's demonstration for Chevron USA. System was restarted May 20, 1992 and optimized according to previously effective system parameters. Mr. Alex Saschin of the BAAQMD was also notified of system non-compliance on May 20.
- j = Contains corrected removal and emission rates and destruction efficiencies.
- k = Destruction efficiency based on FID measurements. The BAAQMD requested the measurements to verify that optimization performed on May 20, 1992 was effective.
- l = Based on vacuum and flow readings from the 6/10/92 site visit.
- m = First day of system operations with the new wells VEW-1 and VEW-2 (installed June 11, 1992) connected to the system as extraction wells.
- n = CR-1 and C-5 disconnected from system to optimize TPH removal rate.
- o = Engine hours upon system start-up on November 2, 1992.
- p = Engine hours immediately prior to system shut down on November 23, 1992.
- q = CR-1 reconnected to the system on January 3, 1993.
- r = Due to FID malfunction or unavailability, PID was used to measure vapor concentrations.
- s = Well gas flow rate estimated based on previous engine data with similar system performance parameters.
- t = Vapor concentrations were too high for PID to measure.
- u = Unable to calculate actual destruction efficiency due to non-detectable concentrations of TPH-G and benzene.
- v = Due to the highly conservative flow rate measured by the ICE flow sensor, the calculated benzene emission rate is higher than the calculated benzene removal rate. The ICE flow sensor measurement has a considerable margin of error and is used as a very conservative estimate of total system flow to account for the small amount of dilution air added by the engine. Because the calculated emission rate was higher than the removal rate, the destruction efficiency could not be calculated.

TPH-G = total petroleum hydrocarbons as gasoline

NA = FID not functioning

<n = analytic result below detection limit of n.

--- = samples not collected

scfm = standard cubic feet per minute

ppm = parts per million on volume to volume basis

Table 2. Total Hydrocarbon Removal, Former Chevron SS#9-4816, 301 14th Street, Oakland, California

Date	Well ID a	Hours of Operation b	Total Well Gas Flow Rate (scfm)		Removal #TPH-G/hr	Interval Average #TPH-G/hr	Interval Hours	Interval Total Pounds TPH-G	Cumulative Total Pounds TPH-G Removed
03/12/92	CR-1/C-5	5	4.9	c	6.54	6.54	5	33	33
03/13/92	CR-1/C-5	23	4.9	c	6.42	6.48	18	117	150
03/16/92	CR-1/C-5	98	4.9	c	5.04	5.73	75	430	580
04/14/92	CR-1/C-5	790	5.1	d	2.71	3.88	692	2,685	3,265
05/12/92	CR-1/C-5	1,465	2.7	d	1.08	1.90	675	1,283	4,548
06/17/92 e	CR-1/C-5	2,071	8.0	d,f	3.21	2.15	606	1,303	5,851
06/19/92	CR-1/C-5/VEW1/VEW2	2,077	25.6	d	3.75	3.75	6	23	5,874
07/20/92	CR-1/C-5/VEW1/VEW2	2,422	31.0	d	3.15	3.45	345	1,190	7,064
08/24/92	VEW-1/VEW-2	3,204	31.4	d	0.45	1.80	782	1,408	8,472
09/21/92	VEW-1/VEW-2	3,852	37.6	d	0.90	0.68	648	441	8,913
10/16/92	VEW-1/VEW-2	4,400	40.0	d,h		0.90	548	493	9,406
11/02/92	VEW-1/VEW-2	4,400	30.2	d,i	3.80	3.80	171	650	10,056
11/09/92	VEW-1/VEW-2	4,571		h					
11/16/92	VEW-1/VEW-2	4,571		i					

--- Table 2 continues on next page ---



Table 2. Total Hydrocarbon Removal, Former Chevron SS#9-4816, 301 14th Street, Oakland, California

Date	Well ID a	Hours of Operation b	Total Well Gas Flow Rate (scfm)		Removal #TPH-G/hr	Interval Average #TPH-G/hr	Interval Hours	Interval Total Pounds TPH-G	Cumulative Total Pounds TPH-G Removed
11/23/92	VEW-1/VEW-2	4,766	35.5	h,j	0.62	0.62	195	121	10,177
12/15/92	VEW-1/VEW-2	4,942	33.0		0.00	0.31	176	55	10,231
01/11/93	VEW-1/VEW-2/CR1	5,255	30.0		1.40	0.68	313	213	10,444
02/08/93	VEW-1/VEW-2/CR1	5,818	18.0		0.22	0.81	563	456	10,900
03/18/93	VEW-1/VEW-2/CR1	6,280	20.1		0.042	0.13	462	61	10,961

Notes:

a = Measurements/samples represent combined extraction from wells listed.

b = Total hours of operation equals engine hours as appear on engine computer printout minus 3050 hours of previous use at other sites.

c = Based on flow data for similar operation parameters, measured vacuum, and assumed influent temperature of 70 F.

d = Based on measured vacuum and flow, and assumed influent temperature of 70 F.

e = First day of system operation with the two new wells (installed June 11, 1992) connected to the system as extraction wells.

f = Based on measured vacuum and flow from the 06/10/92 site visit.

g = Calculated estimates based on concentrations in samples collected 05/12/92.

h = System down upon departure to allow vapors to accumulate in pore spaces.

i = System restarted November 2, 1992. Operation parameters and samples recorded and collected at system stabilization. Removal rate is based on data collected November 2, and is not an interval average.

j = System restarted November 16, 1992. Operation parameters and samples recorded and collected November 23, 1992. Removal rate is based on data collected November 23, and is not an interval average.

SCFM = Standard cubic feet per minute.

ppmv = Parts per million on volume to volume basis.

= Pounds

FID = Total volatile organic compounds (VOCs) as measured by Foxboro organic vapor analyzer/flame ionization device.

TPH-G = Total purgeable hydrocarbons as gasoline.

Table 3. Free Product Thickness, Former Chevron Service Station #9-4816, 301 14th Street, Oakland, California

DATE		C-1	C-2	C-3	C-4	C-5	CR-1	VEW-1	VEW-2	
		<-----product thickness (ft)----->								
11/05/91	a	0	0.04	2.46	0	2.29	2.43			
03/11/92		0	NM	1.09	NM	0.30	3.21			
03/16/92		0	NM	2.32	NM	0	8.88			
03/25/92		0	NM	2.31	NM	0	7.83			
05/05/92		NM	NM	2.11	0	0	5.67			
05/12/92		0	0	1.89	0	0.27	5.97			
05/19/92	b	NM	NM	2.00	NM	NM	2.92			
06/18/92	c	0	0	2.16	NM	0.85	3.12	NM	NM	
07/28/92		0	0	0.51	NM	0	3.41	NM	NM	
08/17/92		0	0	0	0	0	0	NM	NM	
09/15/92		0	0	0	0	0	0	Dry	Dry	
11/02/92		0	0	1.64	0	0	0	Dry	Dry	
11/16/92		NM	NM	1.66	NM	0	1.67	NM	NM	
11/30/92		0	0	1.61	0	0	0.77	Dry	Dry	
12/15/92		0	0	0.8	0	0	0.2	Dry	Dry	
01/04/93		NM	NM	0.6	NM	NM	0	NM	NM	
01/08/93	f	NM	NM	0	NM	NM	0	NM	NM	
01/08/93	g	NM	NM	0	NM	NM	0.01	NM	NM	
01/11/93	h	NM	NM	0.04	NM	NM	0	NM	NM	
01/11/93	i	NM	NM	0.1	NM	NM	0	NM	NM	
01/18/93		0	0	0	0	0	0	NM	NM	
01/25/93		0	0	0	0	0	NM	NM	NM	
02/02/93		NM	NM	0	NM	NM	NM	NM	NM	
02/08/93		0	0	0	0	0	NM	NM	NM	
03/15/93		0	0	0	0	0	0	0	Dry	

Notes:

NM = Not Measured

Dry = Attempted to measure depth to water and free product thickness but the well was dry.

a = From 4th Quarter 1992 Ground Water Monitoring Report prepared by Alton Geoscience, Concord, California

b = Measurement on 5/19/92 was taken prior to free product removal by Erickson Inc. from wells CR-1 and C-3. Erickson vacuumed product from the wells until <1/4 inch remained.

c = VEW-1 and VEW-2 installed June 11, 1992 by Groundwater Technology, Concord, California

d = 1.75 gallons separate-phase product were bailed from well CR-1.

e = About 1 gallon separate-phase product was bailed from well CR-1.

f = FP measured before system shut down.

g = FP measured after system shut down.

h = FP measured before system start-up.

i = FP measured after system start-up.

ATTACHMENT A
ANALYTICAL REPORTS AND CHAIN-OF-CUSTODY FORMS



Superior Precision Analytical, Inc.

1555 Burke, Unit I • San Francisco, California 94124 • (415) 647-2081 / fax (415) 821-7123

C E R T I F I C A T E O F A N A L Y S I S

LABORATORY NO.: 14115
CLIENT: Weiss Associates
CLIENT JOB NO.: 4-582-51

DATE RECEIVED: 02/08/93
DATE REPORTED: 02/10/93
DATE ANALYZED: 02/09/93

ANALYSIS FOR TOTAL PETROLEUM HYDROCARBONS by Modified EPA SW-846 Method 5030 and 8015

LAB #	Sample Identification	Concentration (ppm) Gasoline Range
1	SYS-INF	920
2	SYS-EFF	ND<30

ppm - parts per million in air
Minimum Detection Limit for Gasoline in Air: 30 ppm
Concentration of gasoline in air is calculated based on 20 C
and 1 ATM and an assumed molecular weight of hexane.
Reported as volume to volume.

QAQC Summary:

Daily Standard run at 2mg/L: %DIFF Gasoline = <15
MS/MSD Average Recovery = 83 %: Duplicate RPD = 0%

Richard Srna, Ph.D.


Laboratory Director



Superior Precision Analytical, Inc.

1555 Burke, Unit I • San Francisco, California 94124 • (415) 647-2081 / fax (415) 821-7123

C E R T I F I C A T E O F A N A L Y S I S

LABORATORY NO.: 14115
CLIENT: Weiss Associates
CLIENT JOB NO.: 4-582-51

DATE RECEIVED: 02/08/93
DATE REPORTED: 02/10/93
DATE ANALYZED: 02/09/93

ANALYSIS FOR BENZENE, TOLUENE, ETHYL BENZENE & XYLENES
by EPA SW-846 Methods 5030 and 8020

LAB #	Sample Identification	Concentration(ppb)			
		Benzene	Toluene	Ethyl Benzene	Xylenes
1	SYS-INF	5200	16000	1900	24000
2	SYS-EFF	360	ND<250	ND<65	ND<250

ppb - parts per billion in air

Minimum Detection Limit for Benzene in air = 85 ppb
Minimum Detection Limit for Toluene and Xylenes in air = 250 ppb
Minimum Detection Limit for Ethyl Benzene in air = 65 ppb
Concentration of BTXE in air is calculated based on 20 C and 1 ATM.
Reported as volume to volume.

QAQC Summary:

Daily Standard run at 20ug/L: %DIFF 8020 = <15%
MS/MSD Average Recovery = 82% : Duplicate RPD = 1%

Richard Srna, Ph.D.


Laboratory Director

Chevron U.S.A. Inc.
P.O. BOX 5004
San Ramon, CA 94583
FAX (415)842-9591

Chevron Facility Number 9-4816
Facility Address 310 14th Street, Oakland, CA
Consultant Project Number 4-582-51
Consultant Name WEISS ASSOCIATES
Address 5500 SHELLMOUND ST.
Project Contact (Name) THOMAS BERRY
(Phone) (510) 547-5430 (Fax Number)

Chevron Contact (Name) NANCY VUKELICH VUKELICH
(Phone) (510) 842-9581
Laboratory Name SUPERIOR PRECISION ANALYTICAL
Laboratory Release Number 3523000
Samples Collected by (Name) RONALD C. JENSEN
Collection Date 2/8/93
Signature Ronald C Jensen

Sample Number	Lab Sample Number	Number of Containers	Matrix S = Soil W = Water A = Air C = Charcoal	Type G = Grab C = Composite D = Discrete	Time	Sample Preservation	Iced (Yes or No)	Analyses To Be Performed										Remarks			
								BTEX + TPH GAS (8020 + 8015)	TPH Diesel (8015)	Oil and Grease (5520)	Purgeable Halocarbons (8010)	Purgeable Aromatics (8020)	Purgeable Organics (8240)	Extractable Organics (8270)	Metals Cd, Cr, Pb, Zn, Ni (ICAP or AA)						
SYS-INF		1	A	G	09:30	NONE	N	X													
SYS-EFF		1	A	G	09:40	NONE	N	X													

Please Initial _____
Samples Stored in Ice. NA
Appropriate containers. NA
Samples preserved. NA
COAs without headspace. NA
Comments: _____

Handwritten notes:
2/8/93
15:50

Relinquished By (Signature) <u>Ronald C Jensen</u>	Organization <u>Weiss Assoc</u>	Date/Time <u>2/8/93 15:50</u>	Received By (Signature) <u>J. Howe</u>	Organization <u>Aero</u>	Date/Time <u>2/8/93 15:50</u>	Turn Around Time (Circle Choice) 24 Hrs. 48 Hrs. 5 Days 10 Days <u>As Contracted</u>
Relinquished By (Signature) <u>J. Howe</u>	Organization <u>Aero</u>	Date/Time <u>2/8/93</u>	Received By (Signature)	Organization	Date/Time	
Relinquished By (Signature)	Organization	Date/Time	Received For Laboratory By (Signature) <u>Nancy Retart</u>		Date/Time <u>2/5/93 16:20</u>	

COC-3.DWG/03 01/HCH



Superior Precision Analytical, Inc.

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C E R T I F I C A T E O F A N A L Y S I S

LABORATORY NO.: 14261
CLIENT: WEISS ASSOCIATES
CLIENT JOB NO.: 4-582-51

DATE RECEIVED: 03/19/93
DATE REPORTED: 03/22/93
DATE ANALYZED: 03/19/93

ANALYSIS FOR TOTAL PETROLEUM HYDROCARBONS
by Modified EPA SW-846 Method 5030 and 8015

LAB #	Sample Identification	Concentration (ppm) Gasoline Range
1	SYS-INF	160
2	SYS-EFF	ND<30

ppm - parts per million in air
Minimum Detection Limit for Gasoline in Air: 30 ppm
Concentration of gasoline in air is calculated based on 20°C
and 1 ATM and an assumed molecular weight of hexane.
Reported as volume to volume.

QAQC Summary:

Daily Standard run at 2mg/L: %DIFF Gasoline = <15
MS/MSD Average Recovery = 97 %: Duplicate RPD = 1 %

Richard Srna, Ph.D.

Greg A. Nwomfo
Laboratory Director



Superior Precision Analytical, Inc.

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C E R T I F I C A T E O F A N A L Y S I S

LABORATORY NO.: 14261
CLIENT: WEISS ASSOCIATES
CLIENT JOB NO.: 4-582-51

DATE RECEIVED: 03/19/93
DATE REPORTED: 03/22/93
DATE ANALYZED: 03/19/93

ANALYSIS FOR BENZENE, TOLUENE, ETHYL BENZENE & XYLENES by EPA SW-846 Methods 5030 and 8020

LAB #	Sample Identification	Concentration(ppb)			
		Benzene	Toluene	Ethyl Benzene	Xylenes
1	SYS-INF	1300	2200	150	1300
2	SYS-EFF	720	250	ND<65	ND<250

ppb - parts per billion in air

Minimum Detection Limit for Benzene in air = 85 ppb
Minimum Detection Limit for Toluene and Xylenes in air = 250 ppb
Minimum Detection Limit for Ethyl Benzene in air = 65 ppb
Concentration of BTXE in air is calculated based on 20°C and 1 ATM.
Reported as volume to volume.

QAQC Summary:

Daily Standard run at 20ug/L: %DIFF 8020 = <15%
MS/MSD Average Recovery = 96 % : Duplicate RPD = 4 %

Richard Srna, Ph.D.

Guyn H. ...
Laboratory Director

ATTACHMENT B
SAMPLE EMISSION CALCULATIONS

SAMPLE EMISSION CALCULATIONS
Chevron Service Station #9-4816
301-14th Street
Oakland, California

Given: System data from May 12, 1992

- Influent TPH-G concentration = 30,000 ppmv
- Effluent TPH-G concentration = 450 ppmv
- Influent benzene concentration = 300 ppmv
- Effluent benzene concentration is = 8.1 ppmv
- System vacuum = 38 inches of water
- Molecular weight of TPH-G (assumed to be equal to hexane) = 86 lbs/lb-mole.
- Molecular weight of benzene = 78 lbs/lb-mole
- Extraction flow rate based on the flow sensor and differential pressure gauge located before the ICE. The differential pressure = 0.05
- Emission flow rate is based on measurement by the ICE flow meter. Flow rate = 56.5 cfm

Uncontrolled Emissions (lb per day):

The extraction flow rate is based on measurements using a pitot tube type flow sensor with a differential pressure gauge and an assumed temperature at the sensor of 60°F. The estimated extraction flow rate for the May 12, 1992 data is 2.7 scfm.

The equation for the mass of hydrocarbons entering the treatment system per unit time is:

$$\text{Removal Rate}\left(\frac{\text{lbs}}{\text{day}}\right) = \text{Conc.}(\text{ppmv}) \times 10^{-6} \times \text{flowrate}(\text{scfm}) \times \frac{1\text{lb-mole}}{386 \text{ ft}^3} \times \text{mol. wt.}\left(\frac{\text{lb}}{\text{lb-mole}}\right) \times \frac{1440 \text{ min.}}{\text{day}}$$

For TPH-G and benzene:

$$\text{TPH-G} = 30,000 \times 10^{-6} \times 2.7 \text{ scfm} \times \frac{1\text{lb-mole}}{386 \text{ ft}^3} \times \frac{86 \text{ lbs}}{\text{lb-mole}} \times \frac{1440 \text{ min.}}{\text{day}} = 25.9 \frac{\text{lbs}}{\text{day}}$$

$$\text{Benzene} = 300 \times 10^{-6} \times 2.7 \text{ scfm} \times \frac{1\text{lb-mole}}{386 \text{ ft}^3} \times \frac{78 \text{ lbs}}{\text{lb-mole}} \times \frac{1440 \text{ min.}}{\text{day}} = 0.24 \frac{\text{lbs}}{\text{day}}$$

Controlled Emissions (lb per day):

The emission flow rate is based on the measurement by the ICE flow sensor in cfm, which must be converted to scfm using the following equation:

$$\text{flowrate (scfm)} = \text{flowrate(ICE) (cfm)} \times \left(\frac{14.7 + \text{psig}}{14.7} \right) \times \left(\frac{520}{460 + T_F} \right)$$

where

- T_F = temperature of air in #F,
- $520 = 460 + 60\# =$ standard temperature rankine, and
- $\text{psig} = \frac{\text{inches of water pressure (negative)}}{27.7 \text{ inches of water / 1 psi}}$

So the effluent flow rate is:

$$\text{Flowrate} = 56.5 \text{ cfm} \times \frac{14.7 - \frac{45}{27.7}}{14.7} \times \frac{520}{460 + 70} = 49.3 \text{ scfm}$$

For TPH-G and benzene:

$$\text{TPH-G} = 450 \times 10^{-6} \times 49.3 \text{ scfm} \times \frac{1 \text{ lb-mole}}{386 \text{ ft}^3} \times \frac{86 \text{ lbs}}{\text{lb-mole}} \times \frac{1440 \text{ min.}}{\text{day}} = 7.11 \frac{\text{lbs}}{\text{day}}$$

$$\text{Benzene} = 8.1 \times 10^{-6} \times 49.3 \text{ scfm} \times \frac{1 \text{ lb-mole}}{386 \text{ ft}^3} \times \frac{78 \text{ lbs}}{\text{lb-mole}} \times \frac{1440 \text{ min.}}{\text{day}} = 0.12 \frac{\text{lbs}}{\text{day}}$$

Destruction Efficiency

The equation for destruction efficiency is:

$$\text{Destruction efficiency} = \frac{\frac{\text{lbs removed}}{\text{day}} - \frac{\text{lbs emitted}}{\text{day}}}{\frac{\text{lbs removed}}{\text{day}}} \times 100\%$$

For TPH-G and benzene:

$$\text{TPH-G destruction efficiency} = \frac{25.9 - 7.1}{25.9} \times 100\% = 72.6\%$$

$$\text{benzene destruction efficiency} = \frac{0.24 - 0.12}{0.24} \times 100\% = 50.0\%$$