#### **Harding Lawson Associates**



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April 15, 1993

18106,012.04

Blue Print Service Company 149 Second Street San Francisco, California 94105

Attention: Mr. Jeff Christoff

Gentlemen:

Quarterly Report December 30, 1992 through March 30, 1993 City Blue Groundwater Treatment System 1700 Jefferson Street Oakland, California

This letter presents the current status and discusses the results of sampling and analysis from the groundwater treatment system at the City Blue Production facility at 1700 Jefferson Street in Oakland, California for the period of December 30, 1992 through March 30, 1993.

#### BACKGROUND

Three underground storage tanks were removed from the northwestern portion of the property in June 1987 (Plate 1). Monitoring wells were installed on the property to evaluate the distribution of petroleum hydrocarbons in the soil and groundwater and determine the direction of groundwater flow.

**Petroleum hydrocarbons as gasoline were found floating on the surface of the groundwater in Monitoring Well MW-1.** In January 1988, two additional monitoring wells (MW-1A and MW-4) were installed by HLA at the facility (Plate 1). One offsite monitoring well (MW-5) was installed by HLA in August 1988.

HLA performed additional investigations in 1989 and performed an aquifer testing and groundwater treatment feasibility study in 1990. The groundwater treatment feasibility study identified biodegradation as the most appropriate treatment for the City Blue site.

This quarterly report is the fourth report issued since the system began operating in June 1992. Previous quarterly reports were issued on July 17, 1992, October 13, 1992, and January 20, 1993.

#### **PROCESS DESCRIPTION**

Groundwater containing elevated concentrations of petroleum hydrocarbons as gasoline and non-aqueous phase gasoline (floating product) is being collected from two onsite extraction wells, MW-1A and MW-4. Average system flow rates are 1 to 2 gallons per minute (gpm). Air pumps installed in the wells extract water and convey it April 15, 1993 18106,012.04 Mr. Jeff Christoff Blue Print Service Company Page 2

through aboveground and underground piping to the treatment system. The treatment system is comprised of the following three modules:

Pretreatment: The groundwater and floating product are pumped from the extraction wells to an aboveground oil/water separator. The gasoline is separated from the water and flows to a recovered product tank.

Treatment: The water separated from the gasoline is pumped to a 3,000-gallon biotreatment tank where the water is mixed with nutrient and oxygen to stimulate the growth of microorganisms that degrade the hydrocarbons.

Post-treatment: The contents of the biotreatment tank are pumped through sand filters to remove particulates and activated carbon drums to adsorb the remaining hydrocarbons. Effluent from the activated carbon drums is discharged to the sanitary sewer. Vapor from the bioreactor is passed through a vapor phase carbon adsorption unit before being released to the atmosphere.

Under normal operation, the treatment system processes approximately 1,000 gallons per day. A flow totalizer records the flow in gallons being discharged to the sanitary sewer. Flow totalizer readings are presented in Table 3. Treatment system maintenance must be performed three times a week to maintain continuous operation.

The treatment system has been permitted by the Bay Area Air Quality Management District (BAAQMD), the East Bay Municipal Utilities District (EBMUD), and the Oakland Fire Department.

#### TREATMENT SYSTEM STATUS

On October 24, 1992, a level control switch in the oil/water separator failed, resulting in overfilling of the recovered product tank with gasoline and water. The recovered product tank overflowed into the BPS parking lot and into the street. This incident was reported in the last quarterly report dated January 20, 1993. The level switches failed because they had been fouled by a film of microorganisms and emulsion. The coalescing unit in the separator had also become clogged and had expanded. The coalescing unit was replaced on January 8, 1993.

The treatment system has not been fully operational since October 24, 1993. In the meantime, HLA has performed an engineering evaluation of the treatment system and recommended modifications to improve the safety and maintenance features. The recommended modifications were submitted on April 13, 1993 to BPS and the contractor expected to perform the modifications.

#### TREATMENT SYSTEM SAMPLING

HLA has collected water and air samples from the treatment system. The samples were analyzed by EPA Test Method 8015 for total petroleum hydrocarbons as gasoline (TPH-G) and EPA Test Method 8020 for benzene, toluene, ethyl benzene, and xylenes (BTEX). Water samples were collected from the bioreactor effluent before the carbon beds, CB-1 and CB-2, and from the first carbon bed effluent, CB-1, to monitor for breakthrough of CB-1. In addition, samples of the bioreactor influent have been April 15, 1993 18106,012.04 Mr. Jeff Christoff Blue Print Service Company Page 3

analyzed to determine the degradation efficiency of the bioreactor. Subsequent water sampling will include the effluent from the second carbon bed, CB-2, before the treated water is discharged to the sanitary sewer.

Air samples were collected from the vapor phase carbon bed influent and effluent through the August 20, 1992 sampling. Subsequent air sampling will be from the effluent side only. The sampling locations are shown on Plate 2, Process Flow and Sampling Locations. Water samples were decanted from sampling ports into 40-milliliter volatile organic analysis (VOA) vials. Air samples were collected into 1-liter Tedlar bags with a vacuum box sampler. The air and water samples were stored in coolers on ice and submitted to Superior Analytical Laboratory in San Francisco under chain-of-custody protocols for analysis.

In addition to sampling air and groundwater, the system is maintained and inspected at least twice weekly during normal operation.

#### MONITORING WELL SAMPLING

In accordance with the sampling schedule submitted with the monitoring proposal and regulatory agency permit applications, HLA has sampled the offsite Monitoring Well MW-5 semiannually. The two extraction wells MW-1A and MW-4, and Monitoring Well MW-3 have floating product and have therefore not been sampled semiannually. The results of the MW-5 monitoring are presented in Table 1. The thickness of floating product in the onsite wells is presented in Table 2.

#### SAMPLING SCHEDULE

Air and water samples were collected one hour after the system started on June 16, 1992; every 24 hours for the first three days after the system started; weekly for the first three weeks of operation; and monthly thereafter. When the system is restarted, HLA will monitor the TPH-G and BTEX concentrations in the bioreactor before discharging to the carbon beds and sanitary sewer. The bioreactor influent and effluent and the discharge to the sanitary sewer will be sampled one hour and 24 hours after the system begins discharging to the sanitary sewer. The monthly sampling schedule will resume thereafter.

#### ANALYTICAL RESULTS

A summary of past results of chemical analyses are presented in Table 1. The results indicate that no detectable concentrations of TPH-G or BTEX are in the effluent water being discharged to the sanitary sewer. The bioreactor influent and effluent sample results indicate that the bioreactor treatment has been degrading over 90 percent of the TPH-G and BTEX concentrations before post-treatment polishing by the carbon beds.

The analytical results of the air samples (Table 1) indicate that no detectable concentrations of TPH-G or BTEX have been released from the vapor phase carbon adsorption unit into the atmosphere.

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After the modifications to the treatment system are complete, HLA will train BPS personnel to operate and maintain the treatment system. The analytical results from startup activities and the resumed monthly sampling will be presented in the next quarterly report.

If you have any questions, please contact either of the undersigned.

Yours very truly,

HARDING LAWSON ASSOCIATES

David F. Scrivner Project Engineer

Mark G. Filippini

Engineering Geologist

DFS/MGF/dm/b16954-ct110



Attachments: Laboratory Reports and Chain-of-Custody Records Table 1 - Results of Chemical Analyses Table 2 - Monitoring Well Product Thickness Measurements Table 3 - Flow Totalizer Readings Plate 1 - Site Plan Plate 2 - Process Flow and Sampling Locations

cc: East Bay Municipal Utility District P.O. Box 24055 Oakland, California 94623-1055 Attention: Ms. Molly Ong

> Bay Area Air Quality Management District 939 Ellis Street San Francisco, California 94109 Attention: Mr. Alexander V. Saschin Ms. Loretta Robinson

Alameda County Health Care Services Department of Environmental Health Hazardous Materials Program 80 Swan Way, Room 200 Oakland, California 94621 Attention: Mr. Scott Seery

**Harding Lawson Associates** 

### LABORATORY REPORTS AND CHAIN-OF-CUSTODY RECORDS

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Harding Lav Attn: Dave	wson Asso Scrivne	ociates c		Project 1 Reported	1295-012 04/07/93
		TOTAL PETROLEUM H	YDROCARBONS		
Lab #	Sample	Identification	Sampled	Analyzed	Matrix
56238- 1	MW-5		03/30/93	04/06/93	Water
Laboratory	Number:	RESULTS OF AN 56238-1	ALYSIS		
Gasoline:		74000			
Benzene: Toluene:		16000			
Ethyl Benzer	ne:	1800			
Xylenes:		2700			
Concentratio	on:	ug/L			

Certified Laboratories



CERTIFICATE OF ANALYSIS

### ANALYSIS FOR TOTAL PETROLEUM HYDROCARBONS

Page 2 of 2 QA/QC INFORMATION SET: 56238

NA = ANALYSIS NOT REQUESTED ND = ANALYSIS NOT DETECTED ABOVE QUANTITATION LIMIT ug/L = parts per billion (ppb)

- OIL AND GREASE ANALYSIS By Standard Methods Method 5520F: Minimum Detection Limit in Water: 5000ug/L
- Modified EPA SW-846 Method 8015 for Extractable Hydrocarbons: Minimum Quantitation Limit for Diesel in Water: 50ug/L
- EPA SW-846 Method 8015/5030 Total Purgable Petroleum Hydrocarbons: Minimum Quantitation Limit for Gasoline in Water: 50ug/L
- EPA SW-846 Method 8020/BTXE Minimum Quantitation Limit in Water: 0.3ug/L

ANALYTE	MS/MSD RECOVERY	RPD	CONTROL LIMIT
****			
Gasoline:	95/101	6%	76 <del>-</del> 111
Benzene:	100/101	1%	78-110
Toluene:	103/105	28	78-111
Ethyl Benzene:	107/108	18	78-118
Xylenes:	102/104	28	73-113

Richard Srna, Ph.D.

Certified Laboratories

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	Groundwater Treatment System 1700 Jefferson Street Oakland, California											
Date/ Analytes	Bioreactor Influent (1)	Bioreactor Effluent (2)	First Carbon Bed Effluent (3)	Sanitary Sewer Influent (4)	Vapor Phase Carbon Effluent (Air) (5)	MW-5						
<u>06/16/92</u>												
TPH-G Benzene Toluene Ethylbenzene	NA NA NA	3300 220 460 35	ND<50 ND<0.3 ND<0.3 ND<0.3	NA NA NA	ND<30000 ND<85 ND<250 ND<65	NA NA NA						
<u>06/17/92</u>	NA	290	ND<0.3	NA	ND<250	NA						
TPH-G Benzene Toluene Ethylbenzene Xylene	NA NA NA NA	43000 4900 7600 500 4100	ND<50 ND<0.3 ND<0.3 ND<0.3 ND<0.3	NA NA NA NA	ND<30000 ND<85 ND<250 ND<65 ND<250	NA NA NA NA						
<u>06/18/92</u>												
TPH-G Benzene Toluene Ethylbenzene Xylene	NA NA NA NA	4300 20 48 3.6 970	ND<50 ND<0.3 ND<0.3 ND<0.3 ND<0.3	NA NA NA NA	ND<30000 160 710 89 670	NA NA NA NA						
<u>06/19/92</u>												
TPH-G Benzene Toluene	180000 18000 31000	1600 1.6 5.0	ND<50 ND<0.3 ND<0.3	NA NA NA	ND ND ND	NA NA NA						

ND<0.3

ND<0.3

ND<50

ND<0.3

ND<0.3

ND<0.3

ND<0.3

NA

NA

NA

NA

NA

NA

NA

ND

ND

ND<30000

ND<85

ND<250

ND<65

ND<250

NA

NA

NA

NA

NA

NA

NA

Ethylbenzene

Xylene

<u>06/24/92</u>

TPH-G

Benzene

Toluene

Xylene

Ethylbenzene

2200

16000

NA

NA

NA

NA

NA

ND<0.3

150

980

11

13

1.8

140

#### Table 1. Results of Air and Groundwater Chemical Analysis Groundwater Treatment System 1700 Jefferson Street Oakland, California

Date/ Analytes	Bioreactor Influent (1)	Bioreactor Effluent (2)	First Carbon Bed Effluent (3)	Sanitary Sewer Influent (4)	Vapor Phase Carbon Effluent (Air) (5)	MW-5	
07/02/92							·
ТРН-G	160000	210	ND<50	NA	ND<30000	NA	
Benzene	14000	1.4	ND<0.3	NA	ND<85	NA	
Toluene	27000	ND<0.3	ND<0.3	NA	ND<250	NA	
Ethylbenzene	1700	ND<0.3	ND<0.3	NA	ND<65	NA	
Xylene	1300	1.0	ND<0.3	NA	ND<250	NA	
<u>07/10/92</u>							
трн-д	150000	2800	ND<50	NA	ND<30000	NA	
Benzene	14000	41	ND<0.3	NA	ND<85	NA	
Toluene	26000	36	ND<0.3	NA	ND<250	NA	
Ethylbenzene	1700	2.2	ND<0.3	NA	ND<65	NA	
Xylene	12000	360	ND<0.3	NA	ND<250	NA	
<u>07/17/92</u>							
TPH-G	190000	400	NA	NA	NA	NA	
Benzene	22000	21	NA	NA	NA	NA	
Toluene	34000	25	NA	NA	NA	NA	
Ethylbenzene	2100	0.8	NA	NA	NA	NA	
Xylene	17000	27	NA	NA	NA	NA	
<u>07/24/92</u>							
TPH-G	140000	1100	NA	NA	NA	NA	
Benzene	13000	15	NA	NA	NA	NA	
Toluene	23000	2.4	NA	NA	NA	NA	
Ethylbenzene	1700	ND<0.3	NA	NA	NA	NA	
Xylene	12000	200	NA	NA	NA	NA	
<u>08/20/92</u>							
TPH-G	190000	6400	73	NA	ND<30000	NA	
Benzene	14000	31	ND<0.3	NA	ND<85	NA	
Toluene	24000	14	ND<0.3	NA	ND<250	NA	
Ethylbenzene	2000	ND<6	ND<0.3	NA	ND<65	NA	
Xylene	13000	150	ND<0.3	NA	ND<250	NA	

		,				
Bioreactor Influent (1)	Bioreactor Effluent (2)	First Carbon Bed Effluent (3)	Sanitary Sewer Influent (4)	Vapor Phase Carbon Effluent (Air) (5)	MW-5	
230000	23000	54	NA	ND<30000	NA	
17000	1100	0.4	NA	ND<85	NA	
29000	3600	0.8	NA	ND<250	NA	
2200	59	ND<0.3	NA	ND<65	NA	
15000	1100	0.6	NA	ND<250	NA	
NA	NA	NA	NA	NA	51000	
NA	NA	NA	NA	NA	13000	
NA	NA	NA	NA	NA	5900	
NA	NA	NA	NA	NA	1400	
NA	NA	NA	NA	NA	2600	
NA	NA	NA	NA	NA	74000	
NA	NA	NA	NA	NA	16000	
NA	NA	NA	NA	NA	5000	
NA	NA	NA	NA	NA	1800	
NA	NA	NA	NA	NA	2700	
	Bioreactor Influent (1) 230000 17000 29000 2200 15000 NA NA NA NA NA NA NA NA NA NA NA	Bioreactor Influent (1)Bioreactor Effluent (2)230000 23000 17000 29000 2200 1500023000 1100 3600 299 15000NA 	Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Bed Effluent (3)230000 (2)23000 (3)54 (3)230000 (1)23000 (1)54 (3)230000 (2)23000 (3)54 (3)230000 (1)23000 (1)54 (3)230000 (1)23000 (1)54 (3)230000 (1)23000 (1)54 (3)230000 (1)100 (1)0.4 (3)2000 (1)3600 (1)0.8 (1)2000 (1)3600 (1)0.6NA NA NA NANA NA NA NANA NA NA NANA <b< td=""><td>Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Bed Effluent (3)Sanitary Sewer Influent (4)230000 (1)23000 (2)54 (3)NA (4)230000 (3)23000 (4)54 NA NA NA 2200 100NA NA NA NANA NA</td><td>Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Effluent (3)Vapor Sanitary (4)Vapor Phase Carbon Effluent (Air) (5)230000 (1)23000 (2)54NAND&lt;30000 (4)230000 (1)23000 (2)54NAND&lt;30000 (4)230000 (1)23000 (2)54NAND&lt;30000 (5)230000 (1)23000 (1)0.4NAND&lt;30000 (5)230000 (2)3600 (1)0.4NAND&lt;350 (1)2000 (2)59ND&lt;0.3</td>NAND&lt;250 (2)NA NA NANANANANANA NA NANANANANA NA NA NANANANANA NA NA NANANANANA NA NA NANA NA NANANANA NA NA NA NANA NA NA NANA NA NA NANA NA NA NA NANA NA NA NA NA NA NA NANA NA<br <="" td=""/><td>Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Effluent (3)Vapor Phase Carbon Influent (4)Vapor Phase Carbon Effluent (Air) (5)2300002300054NAND&lt;30000</br></td>NA1700011000.4NAND&lt;85</b<>	Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Bed Effluent (3)Sanitary Sewer Influent (4)230000 (1)23000 (2)54 (3)NA (4)230000 (3)23000 (4)54 NA NA NA 2200 100NA NA NA NANA NA	Bioreactor Influent (1)Bioreactor Effluent (2)First Carbon Effluent (3)Vapor Sanitary (4)Vapor Phase Carbon Effluent (Air) (5)230000 (1)23000 (2)54NAND<30000 (4)230000 (1)23000 (2)54NAND<30000 (4)230000 (1)23000 (2)54NAND<30000 (5)230000 (1)23000 (1)0.4NAND<30000 (5)230000 (2)3600 (1)0.4NAND<350 (1)2000 (2)59ND<0.3	Bioreactor Influent (1)Bioreactor Effluent 

#### Table 1. Results of Air and Groundwater Chemical Analysis Groundwater Treatment System 1700 Jefferson Street Oakland, California

(1) = Sample Location Identification Number (see Plate 2).

All concentrations in parts per billion (ppb).

ND = Not detected above the reporting limit.

NA = Not analyzed.

Date	MW-1	MW-1A	MW-3	MW-4	MW-5
06/18/92	34	NM	NM	NM	NM
07/02/92	18	NM	NM	NM	NM
07/23/92	10	NM	NM	NM	NM
08/18/92	10	NM	NM	NM	NM
09/30/92	NM	NM	4.1	NM	0
11/11/92	13	NM	2	NM	NM
01/29/93	25.2	NM	1.7	NM	NM
02/12/93	10.2	13	1.3	8.8	0
03/30/93	NM	NM	NM	NM	0.06

Table 2. Monitoring Well Product Thickness Measurements

All measurements in inches.

NM = Not measured

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Date	Flow Total to Sanitary Sewer (gallons)	
06/16/92 06/17/92 06/18/92	1,000 2,957 4,011	
06/19/92 06/24/92 07/02/92	5,650 6,830 13,040	
07/10/92 07/24/92 09/15/92	14,470 19,450 51,190	
10/15/92 10/23/92	70,370 75,470	

# Table 3. Flow Totalizer ReadingsDischarge to Sanitary Sewer



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